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# Key factors influencing the environmental performance of pyrolysis, gasification and incineration Waste-to-Energy technologies

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## ABSTRACT

Waste-to-Energy (WtE) has started playing an increasingly important role in the recovery of energy from municipal solid waste (MSW). A number of WtE technologies are being developed. However, selecting a more environmentally sustainable option is difficult due to data limitation and methodological inconsistencies. Using life cycle assessment (LCA) as a tool, this paper aims to identify key factors influencing the potential environmental impacts of four representative WtE technologies, namely the incineration (S1), pyrolysis (S2), gasification (S3), and gasification coupled with ash melting (S4). The systems are constructed using inventory data based on on-site operation of several industrial-scale reference plants. A comprehensive sensitivity analysis is conducted, assessing a range of critical input parameters, processes, operating conditions and modelling assumptions. The results demonstrate that all analysed WtE systems exhibit environmental benefits (i.e. negative environmental impacts) for most of the impacts, while S3 seems to be more optimal due to an intermediate syngas cleaning process, which results in both reduced emissions and increased energy recovery. Parameters driving the environmental impacts are energy recovery efficiency, feedstock variability, NO<sub>x</sub> and CO<sub>2</sub> emissions at stack, and recycling of metals. Moreover, the overall ranking of different WtE systems is strongly dependent on operating conditions, such as effectiveness of the air pollution control process, utilization pathway of pyrolysis char, and to a lesser extent, bottom ash management (landfill or recycling). The LCA modelling conditions, such as substituted source of electricity, choice of functional unit and time frame are also shown to significantly affect the quantified environmental performance. Finally, the study highlights the directions, towards which, efforts should be focused throughout all stages of each WtE technology to obtain further improvements.

### Keywords:

Waste-to-Energy  
Energy conversion technologies  
Energy recovery  
Life cycle assessment  
Environmental impacts  
Optimization

## 1. Introduction

Waste-to-Energy (WtE) has played an important role in dealing with the increasing production of municipal solid waste (MSW) [1]. Stimulated by dwindling reserves of fossil fuels and sustainable energy production, WtE is seen as an attractive approach to recover energy and useful materials [2]. Today, approximately 1.5% of the total energy is provided by WtE in European Union (EU) [3]. In this context, the future goal of modern WtE has shifted from being a “waste treatment sector” to an “energy and resource producer” [4].

Incineration is currently the most mature WtE technology with over 1400 plants in operation around the world [5]. The last generation of incinerators is equipped with advanced air pollution control (APC) system, which has significantly improved their environmental performance [6]. Pyrolysis and gasification are newly developed WtE

technologies [7], which operate in the absence of oxygen (pyrolysis) or in the presence of sub-stoichiometric air (gasification) to yield syngas ahead of combustion (the process is called the “two-step oxidation”). Both processes offer opportunities to minimize the formation of dioxins and to integrate with high-efficient energy recovery devices (such as, gas turbines and gas engines). So far, pyrolysis/gasification-based WtE is still less applied on commercial scale, as around a hundred plants are reported to process MSW [8].

However, there remains a lack of consensus about a better WtE technology. From the perspective of environment, WtE should achieve lower emissions, a higher energy recovery efficiency, and efficient recovery of inorganic materials. Therefore, it is necessary to conduct a systematic comparison among various WtE technologies.

This targeted aim calls for support by suitable assessment tools. Life cycle assessment (LCA) represents a comprehensive methodology as it

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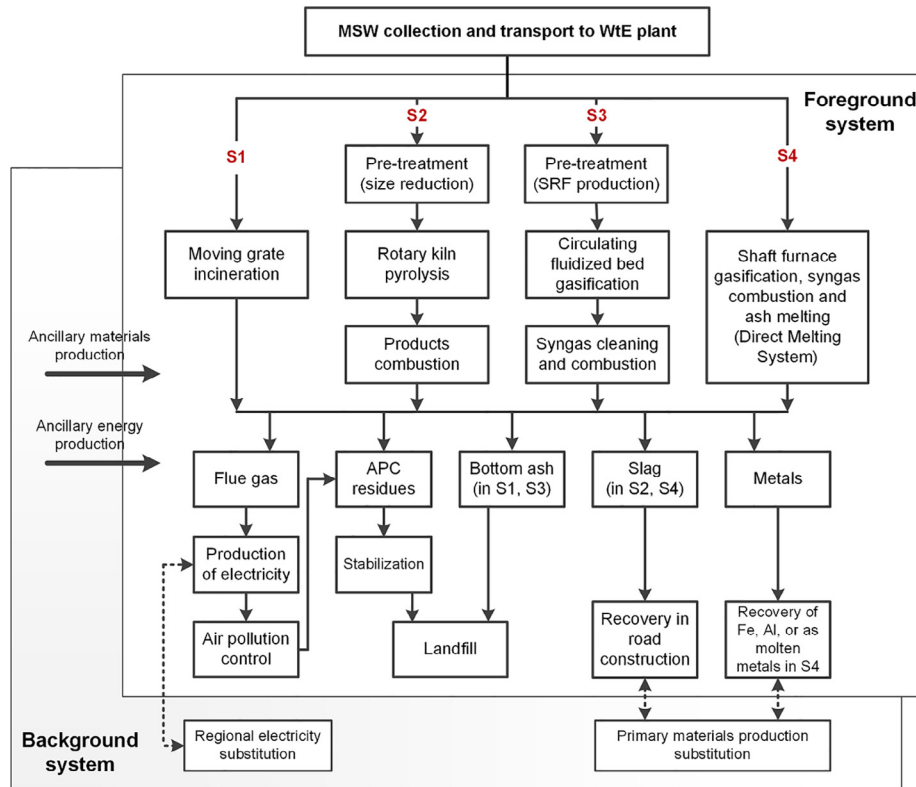


Fig. 1. System boundaries of LCA model.

quantifies both direct and indirect environmental impacts of a system throughout its life cycle [9,10]. In the past years, increasing LCA studies have been performed in the field of WtE. Majority of these studies are focused on incineration, aiming at identifying potential environmental burdens [11,12], or making comparisons with alternatives such as landfill [13,14]. However, LCA of pyrolysis and gasification technologies is still scarcely assessed. Evangelisti [15] evaluated three pyrolysis and gasification systems (gasification-plasma gas cleaning, pyrolysis-combustion, and gasification-combustion) and reported that gasification-plasma was the only system showing a better environmental performance over modern incineration. Zaman [16] in turn indicated that gasification-combustion appeared more optimal than incineration. The contradictory result to those of Evangelisti [15] can be mainly due to different energy recovery efficiencies adopted in these studies. Arena [5] compared operational data from a gasification-melting system with incineration and reported that incineration was better for most of the selected impact categories, though gasification could produce a less leachable residue with a greater potential to be recovered. Overall, as highlighted by Khandelwal [17] and Mayer [3] in recent reviews, a comparison of different WtE technologies requires further investigation to derive clearer results.

The inconsistencies in the available literature can be explained by issues of both WtE technical parameters and LCA modelling methodologies [9]. From the technic perspective of WtE, existing studies revealed that parameters, such as plant energy efficiencies [18], air pollutants at stack [19], waste composition [20], and solid residues management [21] were decisive for environmental performance. Besides, LCA principles, such as energy substitution [22], temporal and geographic horizon [23], and choices of impact assessment methods [24] were also proven to be vital factors affecting the life cycle impacts. However, very few of the studies (i.e. only 6% of 315 peer-reviewed studies [3]) have addressed the holistic description of all these aspects, which has hindered transparent comparison and determination of a more sustainable WtE technology.

Consequently, this paper aims to give a systematic assessment of

environmental profile of different WtE technologies. Within this context, first, an LCA modelling is conducted quantifying the environmental impacts of four WtE technologies, namely incineration, pyrolysis, gasification and gasification-melting. This is done based on data inventory from on-site operation of several representative plants. These technologies are the most common types of WtE currently available. Then, the results are discussed by a comprehensive sensitivity analysis to seek crucial factors (i.e. input parameters, processes, operating conditions, and modelling assumptions), which drive their environmental sustainability. Finally, potential areas of improvement are outlined for each specific technology. Therefore, this paper contributes to already existing LCA and extends knowledge in the following ways: (1) quantifying the environmental performance of different WtE technologies, which fills the knowledge gaps in this field and also serves as a reference for other similar LCA studies; (2) carrying out a holistic sensitivity analysis of the LCA process, which identifies key environmental hotspots and bottlenecks of each WtE technology for future improvements; (3) the results from this study are expected to increase the credibility and reliability of LCA, thus providing potentially useful recommendations for public policy and planning.

## 2. Methodology

### 2.1. Goal and scope definition

The life cycle assessment is performed following the ISO standards [25] and the International Reference Life Cycle Data System (ILCD) Handbook [26]. The aim is to compare the environmental impacts of four representative WtE technologies, and then, to identify the key factors determining their sustainability as well as potential areas of improvements. The goal of this study is in accordance with the “Situation C1” as defined by the ILCD Handbook, and implies an “attributional” approach for LCA modelling. The LCA modelling is carried out by using the Gabi 8.0 software.

Fig. 1 shows the system boundaries under consideration, which are

split into foreground and background systems. The foreground system covers waste pre-treatment (required in several WtE units), thermal conversion (incineration, pyrolysis, gasification, or gasification-melting), energy recovery, APC, and solid residues management. MSW collection and transportation before arriving the WtE plants are not included. All plants are assumed to be connected to steam turbine for energy recovery and are equipped with a typical APC line comprising selective non-catalytic reduction (SNCR), dry scrubber with slaked lime ( $\text{Ca}(\text{OH})_2$ ) and activate carbon, and bag filter for removing  $\text{NO}_x$ , acid gases, dioxins, and particulate matter (PM). Solid residues include bottom ash, slag and APC residues. It is worth noticing that the bottom ash (generated in S1, and S3 scenarios) and slag (generated in S2, and S4 scenarios) are separately defined due to their different characteristics. The latter appears as a melted, vitrified material feasible for immediate recycling [27]. Instead, the bottom ash is assumed to be landfilled, which follows the common EU practice. APC residues mainly consist of fly ash and exhausted sorbents, and are stabilized before final disposal in landfill at a distance of 200 km. It should be mentioned that these settings are used in the baseline cases (default situation), while among these input parameters, the most critical ones will be discussed in detail based upon a sensitivity analysis, which is discussed in a later section 2.4.

Based upon the data from the Gabi databank, the background system quantifies the upstream production of ancillaries, as well as the benefits from recovered energy, metals and inerts. The plants are considered to produce electricity only. This assumption makes the modelling easier and would not affect the comparison results [5]. In appliance with the attributional LCA, the “multifunctional” issue is addressed based upon the system expansion. The recovered electricity is assumed to substitute an equivalent amount of electricity from EU grid mix (25.8% nuclear, 21.5% coal, 19.7% natural gas, and 30.2% renewables, as par 2016 statistics) [28]. The recycling of metals is credited for avoiding the production of virgin metals. The recovered slag is used in road construction to substitute natural aggregates.

The functional unit is defined as the thermal treatment with electricity recovery of one tonne of MSW. The plants are assumed to be located in EU, and have a composition of the EU average residual waste (Table 1) [29], and a lower heating value of 10.307 GJ/tonne according to the CEWEP report of 314 waste incineration plants in EU [30]. The elementary composition is determined for each waste fraction based on the study of Koehler [31] (see Table S1 in Supplementary Material). The LCA time frame for potential environmental impacts is considered to be 100 years. This is in particular relevance for the leaching of ash components in landfill, where emissions can last thousands of years [9,11]. A long-term perspective covering a time span of 60,000 years will be discussed in the sensitivity analysis, which is based upon recommendations of Doka [23].

**Table 1**  
EU average Municipal solid waste composition assumed as reference for the LCA modelling.

Waste composition	Content (wt%, as received basis)
Organic waste	35
Paper	20
Plastics	11
Textiles	4
Glass	5
Metals	3
Other/inert waste <sup>a</sup>	22

<sup>a</sup> “Other/inert waste” may include amounts of combustibles that not elsewhere classified. However due to the lack of data, this composition is treated as a whole as non-combustible.

## 2.2. Data source and inventory analysis

The LCA modelling is processed using mass and energy balances, which is based upon the material and substance flow analysis (MFA/SFA) for each WtE system. The incoming waste can end up in any of the compartments, including bottom ash (or slag), APC residues, or airborne emissions. Transfer coefficients (TCs) express the proportion of each input element constituting the waste. The source and data used to compute TCs are detailed in the Supplementary Material (Section SM-2). Fig. 2 shows the mass flow sheets in the four analysed WtE systems.

The data used are mainly based on on-site operation of several reference plants. The selected plants are all industrial-scale, and therefore, are capable of reflecting reliable and representative performance of specific WtE technologies. Basic information of the reference WtE plants is provided in Table 2. It is worth noticing that the selected gasification-melting plant is located in Japan, which may result in a different waste composition from that in EU. However this would not cause significant effects on the operating of gasification-melting process, such as coke consumption [32]. The life cycle inventory is summarized in Table 3, while the description of each scenario is detailed as follows.

### 2.2.1. S1: Incineration

The modelled incineration reflects moving grate incinerator, which is the predominant type used worldwide [19]. TCs for incineration are adapted from the work of Koehler [31]. The process conditions are sourced from the average performance of 110 incineration plants (85% of the total number) operating in France [33,34]. Therefore, the data are representative of incineration in other regions with similar technology levels.

Air emissions are divided into two categories, namely the waste-specific and process-specific emissions. Waste-specific emissions are dependent on waste input and are calculated using TCs. Two pollutants ( $\text{CO}_{2,\text{fossil}}$  and Hg) are compiled considering the availability of TCs relative to each WtE system. Process-specific emissions are controlled by thermal technologies and/or APC operation. Seven pollutants (CO, dioxins, HCl,  $\text{NH}_3$ ,  $\text{NO}_x$ , PM and  $\text{SO}_2$ ) are considered, which are calculated using emission factors based on French incinerators.

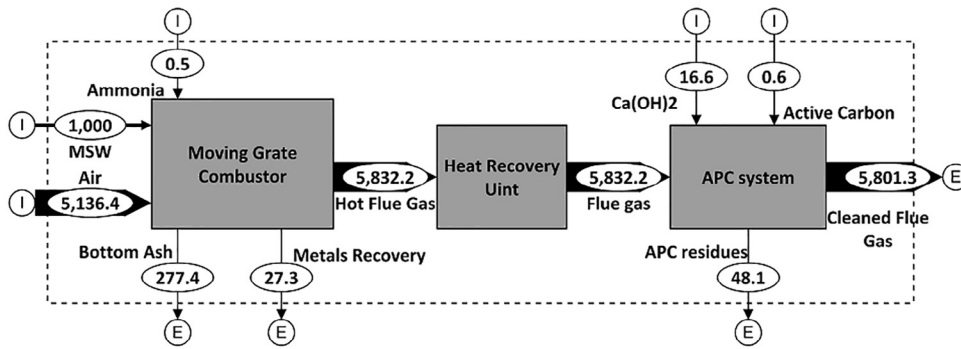
Incineration enables the recovery of energy and materials. A net electricity recovery efficiency of 17.7% is used, which is reported by CEWEP as an average value for the selected incineration plants in EU [30]. The mass and composition of bottom ash and APC residues are calculated using TCs. Scrap metals in the bottom ash can be recovered using mechanical separation. The processing steps and associated energy consumptions are sourced from the work of Allegrini [21]. A typical recovery efficiency of 80% is used for ferrous (Fe) scraps [11]. While the recovery of non-ferrous scraps varies with technologies, Aluminium (Al) recovery with a typical efficiency of 30% is considered [11]. The remaining bottom ash is landfilled, whereas the modelling of the leaching of ash elements is taken from the work of Doka [23]. The APC residues are assumed to be chemically stabilized by the Ferrox process. A detailed assessment of the associated impacts is estimated according to Fruergaard [35].

### 2.2.2. S2: Pyrolysis

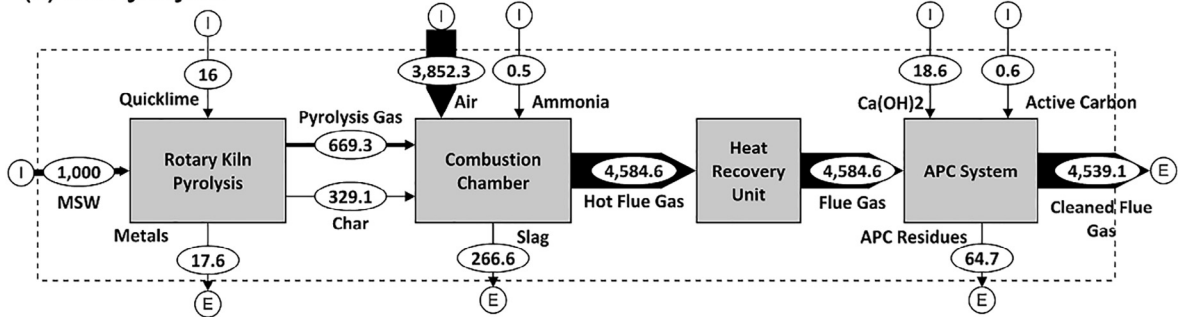
The modelling of pyrolysis is based on rotary kiln, which is the only type of reactor that has successfully achieved industrial-scale implementation [36]. The basic processes and data are calculated from the reference plant “Burgau” in Germany [37], which had operated for over 30 years (until 2015) and is a good example of full-scale pyrolysis. The associated TCs are approximated based upon the work of Arena and Di Gregorio [38], which have been adapted considering data of air emissions in the reference plant.

The incoming waste is shredded to 300 mm size as a pre-treatment step, and is then fed into the rotary kiln together with around 12–20 kg of quicklime per tonne of waste [39]. The kiln is externally heated using

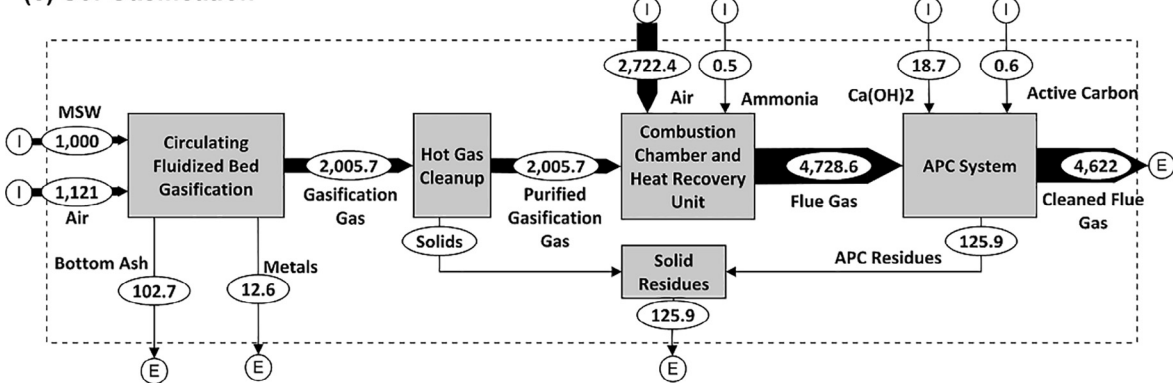
**(a) S1: Incineration**



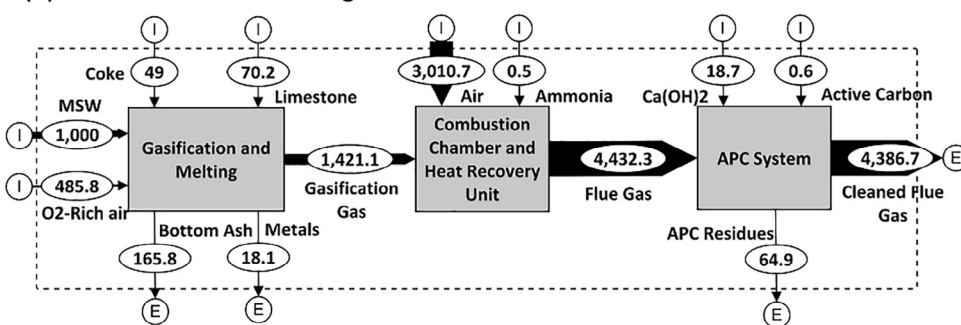
**(b) S2: Pyrolysis**



**(c) S3: Gasification**



**(d) S4: Gasification-melting**



**Fig. 2.** Configuration and mass flows in the four different WtE technologies. Data are adjusted to the functional unit of 1 tonne of MSW, values are expressed as kg. Letters “I” and “E” represent respectively “import” and “export”.

combustion flue gas to maintain the core reaction zone at about 500 °C. Pyrolysis is carried out with an average residence time of 1 h, due to which, the waste is converted into gas and char fractions. The gas is conveyed to a downstream combustor, which operates at 1200 °C. The solid fraction undergoes separation to extract metals. Their recovery

efficiencies are assumed to be same as those of incineration. The remaining char in Burgau plant is not utilized and is transported to landfill. However, it should be noted that this reference plant was designed for pure disposal purpose at the time of planning. Since the aim of this study is to examine the waste-to-energy potential of different

**Table 2**  
Reference WtE plants considered in this study.

Scenario	Technology	Type (supplier)	Feedstock	Plant capacities (tonnes/year)	Reference plants
S1	Incineration	Moving grate	Residual MSW	10,000–700,000	110 French incineration plants [33,34]
S2	Pyrolysis	Rotary kiln	MSW, industrial waste, sewage sludge	35,000	Burgau, Germany [37,39]
S3	Gasification	Circulating fluidized bed	Solid Refuse Fuels	250,000	Kymijärvi II, Finland [40,44]
S4	Gasification- melting	Direct Melting System (shaft furnace)	MSW	75,000	A specified plant in Japan [27,32,45]

technologies, proper utilization of this high-caloric char should be considered, as it would have a significant impact on the overall energy efficiency. As a result, char is assumed to be milled to fine powders, and combusts along with syngas, following common practices in similar plants (such as, Siemens, Mitsui, and Takuma). The temperatures of the combustion chamber are sufficiently high, which generates a molten slag. As mentioned previously, the slag can have a superior leaching resistance, due to which, it is regarded as a recyclable material for road construction application.

### 2.2.3. S3: Gasification

The modelling of gasification is based on the operation of reference plant “Kymijärvi II” in Finland [40], which uses circulating fluidized bed gasifier and is the largest gasification plant processing MSW-derived fuels (namely, solid refuse fuels; SRF) in the world. The TCs have been estimated based on the studies of Konttinen [41] and Arena and Di Gregorio [42].

The MSW is upgraded (through shredding, and pelletization) to accord with the required quality of SRF. Such processing requires energy and the data are taken from Nasrullah [43]. Then, the waste passes into the gasifier, which operates at 850–900 °C to generate syngas. This is followed by gas cleaning, for which the produced gas is cooled in a heat recovery unit the temperature drops down to 400 °C. After this, the gas passes through a series of ceramic filters to remove alkalis, heavy metals and PM. The cleaned syngas has few corrosive contaminants, which enable it to produce high-quality steam (540 °C, and 121 bar). This steam quality is higher than those produced in conventional incineration plants (40 bar, 400 °C) [44]. Consequently, the plant reaches an electricity recovery efficiency of 27.4% (net efficiency) [40]. The produced bottom ash appears similar to that from the incineration case, which is landfilled after recycling of the metals.

### 2.2.4. S4: Gasification-melting

The Direct Melting System, which has achieved commercial operation for more than 30 years in Japan and South Korea, is selected as a representative gasification-melting system. The performance data are mainly sourced from a reference plant in Japan, which is one of the world’s largest gasification-melting plants [27,32,45]. The TCs are taken from Arena and Di Gregorio [38] based on a similar prototype.

The MSW does not require pre-treatment. It is fed into the shaft furnace together with coke (to assist ash melting) and limestone (to adjust the viscosity of melt). Gasification occurs in the middle zone of the furnace (600–800 °C) and the produced syngas is sent for complete burning in a downstream combustor. Incombustible waste fractions descend to the bottom of furnace, where combustion and melting reactions occur with the injection of O<sub>2</sub>-rich air (36 vol% O<sub>2</sub>) at 1000–1800 °C. Molten residues are discharged intermittently and separated magnetically into slag and metals. The net electricity recovery efficiency reaches 16.7% by subtracting the internal power consumption, such as oxygen generator and ash melting [32].

## 2.3. Life cycle impact assessment

The life cycle impact assessment (LCIA) is estimated according to the CML 2001 method, updated in August 2016. A total of 11 impacts including both toxic and non-toxic categories are considered: global warming (GWP), acidification (AP), eutrophication (EP), ozone layer depletion (ODP), photochemical ozone creation (POCP), terrestrial ecotoxicity (TETP), freshwater aquatic ecotoxicity (FAETP), human toxicity (HTP), marine aquatic ecotoxicity (MAETP), and abiotic depletion (ADP elements and ADP fossil). The accounting of biogenic CO<sub>2</sub> emissions (as opposed to CO<sub>2</sub> where the carbon is of fossil origin) are widely debated. In this study, biogenic CO<sub>2</sub> is treated carbon neutral (GWP of zero), following currently common LCA practice [46,47].

**Table 3**

Life cycle inventory table for the four different WtE technologies, referred to the functional unit of 1 tonne of MSW.

	Unit	Incineration(S1)	Pyrolysis(S2)	Gasification(S3)	Gasification-melting (S4)
<b>Input streams</b>					
Limestone as ancillary material	kg	-	-	-	70.20
Quicklime as ancillary material	kg	-	-	-	16.00
Coke as ancillary fuel	kg	-	-	-	49.00
Electricity for MSW pre-treatment	kwh	-	- <sup>a</sup>	70.00	-
Slaked lime for APC	kg	16.63	18.58	18.71	18.70
Ammonia for APC	kg	0.52	0.52	0.52	0.52
Active carbon for APC	kg	0.56	0.56	0.56	0.56
<b>Output solid residues to be treated</b>					
Bottom ash, to be landfilled <sup>b</sup>	kg	277.43	-	102.73	-
APC residues, to be stabilized followed by landfill	kg	48.09	64.72	125.93	64.90
<b>Direct emissions to air</b>					
CO <sub>2,fossil</sub> <sup>c</sup>	kg	416.97	419.92	419.95	602.29
CO	g	35.11	49.28	9.86	35.43
HCl	g	31.07	25.13	4.93	21.15
NH <sub>3</sub>	g	24.64	24.64	24.64	28.57
NO <sub>x</sub>	g	763.17	822.52	793.44	120.01
PM <sup>d</sup>	g	5.68	6.90	9.86	12.57
SO <sub>2</sub>	g	40.46	39.43	34.50	18.86
Hg	g	3.14E-02	5.42E-02	4.93E-04	9.86E-02
Dioxins	g	4.51E-08	4.93E-09	9.86E-09	4.97E-09
<b>Recovered streams (avoided burdens)</b>					
Net electricity output	kwh	506.76	593.17	783.49	558.90
Slag for road construction	kg	-	266.56	-	165.76
Ferrous scrap	kg	15.46	10.76	7.98	-
Aluminium scrap	kg	11.83	6.82	4.64	-
Molten metals	kg	-	-	-	18.06

APC = air pollution control, PM = particulate matter

<sup>a</sup> The raw MSW need to be shredded as pre-treatment in pyrolysis scenario (S2), which necessarily requires electricity. The consumption amount, together with the energy required for char milling, has been quantified as a whole (i.e. internal energy use, assumed to be 20% of the total recovered electricity).

<sup>b</sup> The value presents the net amount of bottom ash after metals separation, which is destined to be landfilled.

<sup>c</sup> Biogenic CO<sub>2</sub> emissions are considered neutral to GWP. The fraction of biogenic carbon based on EU average MSW composition is estimated at 48% according to IPCC guideline.

<sup>d</sup> The PM emission is divided into 99.5% PM<sub>2.5</sub> and 0.5% PM<sub>2.5-10</sub> according to Doka [23], with the aim to better quantify its impact on human and ecosystem.

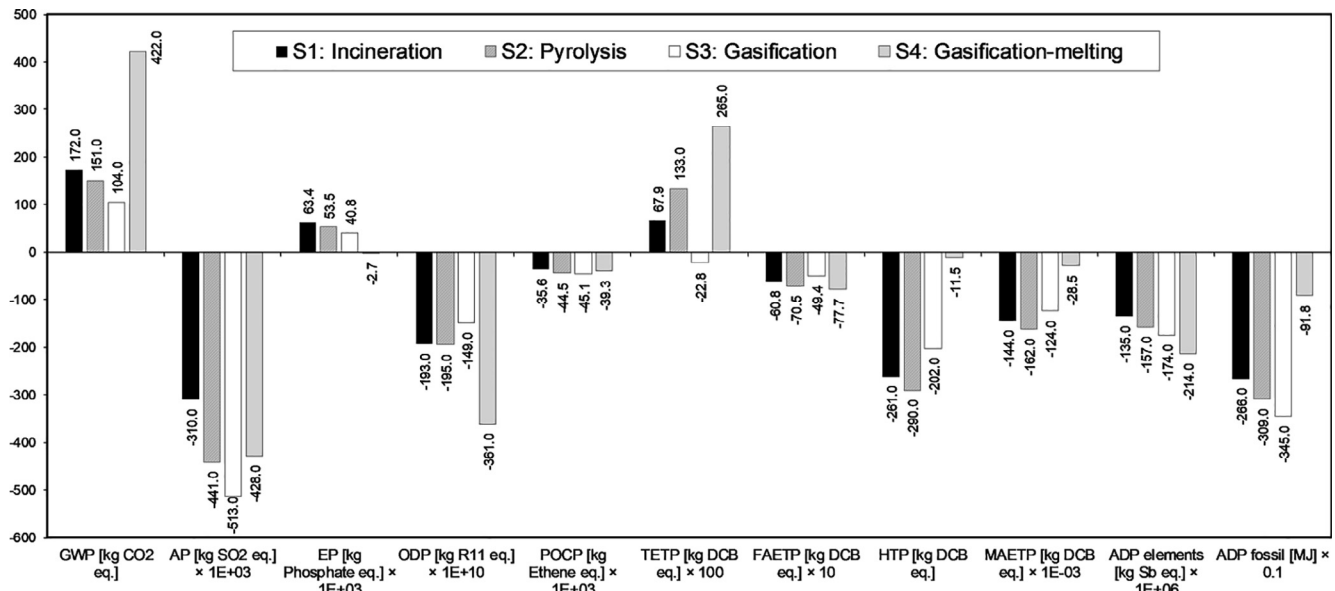


Fig. 3. Characterized results of impact assessment for the treatment of 1 tonne of MSW using four different WtE technologies. Some impacts are scaled to fit the y-axis; their original values can be obtained by dividing the factor shown on the x-axis.

#### 2.4. Sensitivity analysis

The sensitivity analysis is conducted using the method recommended by Clavreul [48]. The objective is to systematically identify key factors influencing the environmental performance of different WtE systems. The following steps have been applied successively.

- Perturbation analysis identifies important individual parameters to overall results, whereby all input parameters are varied one at a time by 10% by the following equation:

$$SR = \frac{\frac{\Delta result}{initial result}}{\frac{\Delta parameter}{initial parameter}} \quad (1)$$

where SR is the sensitivity ratio;  $\frac{\Delta result}{initial result}$  is the relative change of the total result;  $\frac{\Delta parameter}{initial parameter}$  is the relative change of an individual parameter. A list of the tested parameters in each scenario is presented in the [Supplementary Material \(Table S8\)](#). Parameters with a higher absolute SR represent that they have more significant influence on the overall results. Parameters with SR values higher than 0.2 will be further discussed.

- Several process operating conditions are then discussed based upon the scenario analysis. The aim is to examine if an alternative choice for the construction of scenarios would vary the ranking of WtE systems or not.
- The last part of the sensitivity analysis addresses model assumptions. From the methodological point of view, the LCA results typically depend on various choices. Three critical aspects, namely the substituted energy sources, the choice of a functional unit, and the choice of time frame, are discussed herein.

### 3. Results

The overall environmental impacts of the baseline WtE systems are shown in [Fig. 3](#). All the four systems exhibit negative values for 8 out of 11 impacts, indicating an environmental benefit due to credits from the recovery of energy and materials. Contrarily, positive values of GWP, EP and TETP impacts indicate environmental burdens. Comparing different WtE technologies, gasification (S3) is better for 5 impacts (GWP, AP, POCP, TETP, and ADP fossil). Gasification-melting (S4) instead has the lowest impacts in 4 categories (EP, ODP, FAETP, and ADP elements), whilst pyrolysis (S2) is superior for HTP.

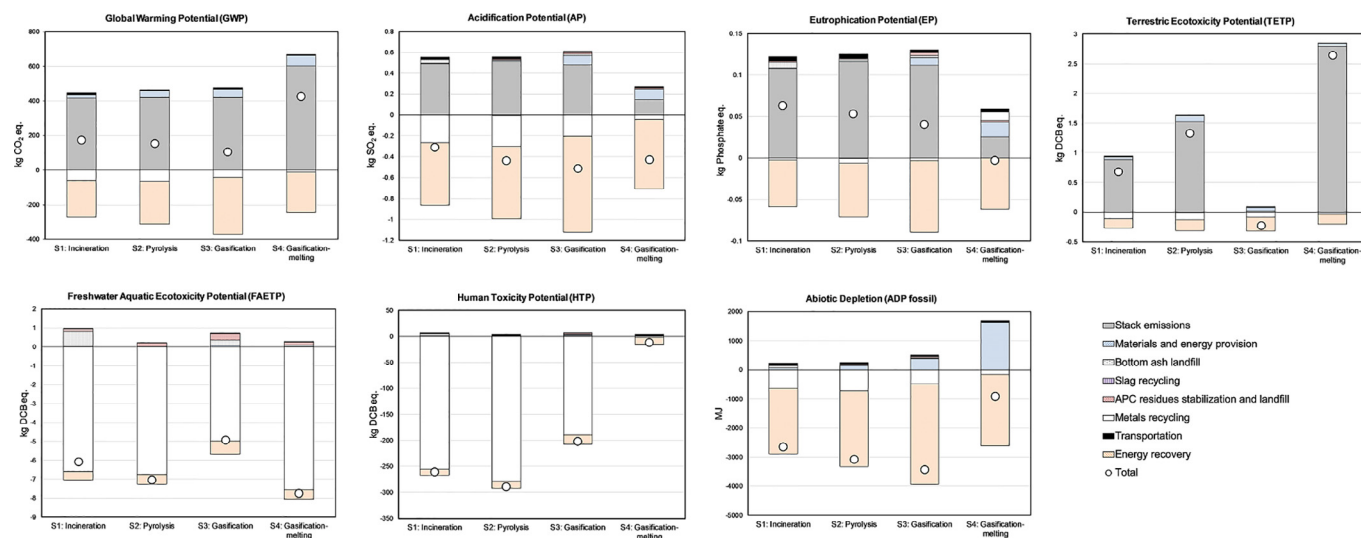
In order to identify main sources of the environmental burdens, contribution analysis is conducted to distribute the overall impacts into different life cycle stages. [Fig. 4](#) reports the results refer to 7 selected categories that are representative in terms of non-toxic impacts, toxic impacts and resources depletion. It is observed that the impacts from “stack emissions”, “energy recovery” and “metals recycling” are the most noteworthy contributors, with the former one being an environmental loading and the latter two being environmental savings. The “stack emissions” account for a large proportion of the GWP, AP, EP and TETP impacts. For all WtE systems there is a positive impact of GWP, which is mainly due to the fossil-origin CO<sub>2</sub> emission derived from MSW. S1, S2 and S3 scenarios show negligible difference of GWP stack emissions (417–420 kg CO<sub>2</sub> eq.), while that value in S4 is much higher

(602 kg CO<sub>2</sub> eq.) due to the burning of coke to maintain high temperature in the melting zone of the gasifier [27]. By contrast, S4 shows a significantly lower AP and EP emissions at stack, of which NO<sub>x</sub> emission is the principal contributor. The reduced impacts can be ascribed to the following two reasons. Firstly, the emissions data in specified WtE plants are broadly comparable with the exception of NO<sub>x</sub> (Table 3), of which S4 shows the lowest NO<sub>x</sub> emission. Secondly, pyrolysis and gasification WtE produces a lower flue gas volume as a consequence of the lower excess air (ER = 1.2 vs. ER = 1.6 in S1). Hence, mass emission rate per tonne of MSW is decreased compared with incineration. Lastly with respect to TETP, heavy metals (here only Hg is considered) are the major contributors. S3 shows the least impact due to intermediate gas cleaning that has condensed part of the metals in the filter.

“Energy recovery”, due to the substitution of fossil fuels combustion for electricity production, has made a significant contribution to reduce GWP, AP, EP and ADP fossil impacts. The highest avoided emissions are found in S3. As has been mentioned previously, the use of intermediate syngas purification offers the opportunity to remove targeted pollutants (particularly Cl) prior to combustion. In this case, the steam data of the boiler reach 121 bar and 540 °C, thus improving the efficiency of the power cycle (a net efficiency of 27% in S3 vs. 18% in S1). On the other hand, S4 shows the lowest amount of electricity recovered. This is because the ash melting process is quite energy intensive, which consumes about 24% of the gross electricity generated. However, the main advantages of melting are size reduction of the ash to be landfilled and the decrease of toxicity (dioxins and heavy metals leaching) [49].

“Metals recycling” shows also avoided impacts, in particular for toxicity impacts (FAETP, HTP). Recycling of Fe is the main contributor to FAETP credits (greater than 96%), while HTP credits are nearly completely ascribed to Al recycling. This indicates that the environmental impacts from scrap metals separation, upgrading, and re-processing are considerably lower than their production from virgin materials [11]. With reference to the four WtE scenarios, the composition of recycled metals is strongly different, mainly as oxidized form in incineration and metallic form in pyrolysis and gasification. Higher actual recovery efficiencies and subsequently increased avoiding impacts are thus possible in pyrolysis/gasification-based WtE. However, S3 shows lower FAETP and HTP credits due to higher transfer of metals to fly ash (see [Table S4](#)).

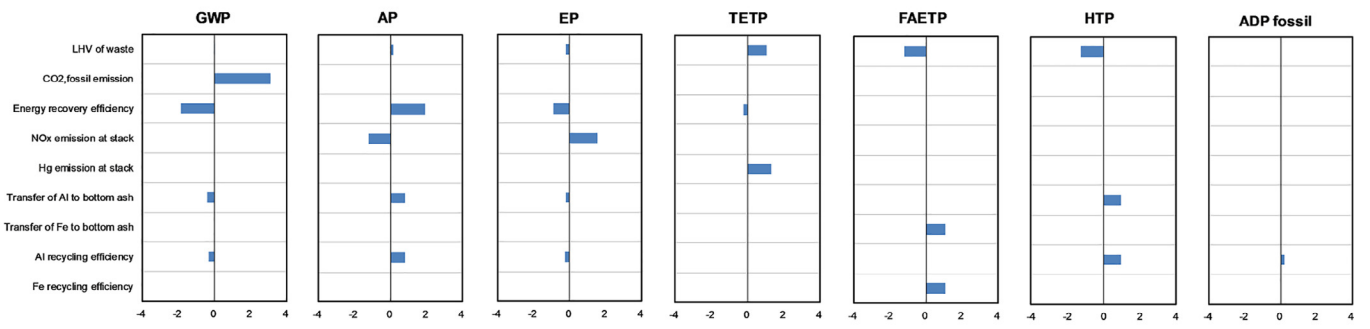
“Materials and energy provision” have only a minor contribution to S1 and S2 scenarios, however is more noteworthy in S3 and S4. For S3 this contribution mainly derives from the energy demand to produce



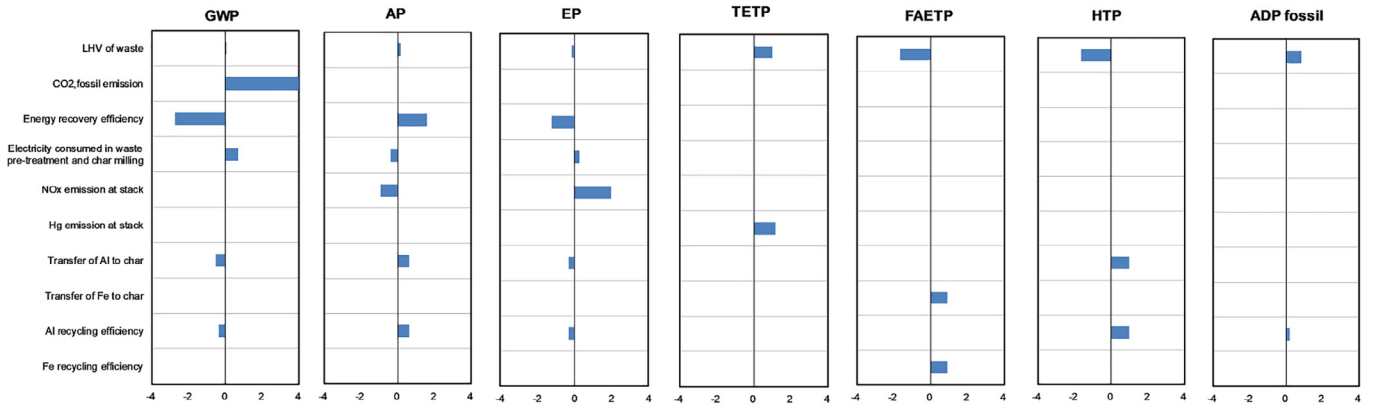
**Fig. 4.** Contribution analysis of different life cycle stages to the impacts from the four different WtE technologies. Only selected impact categories are shown in the figure, the impacts are estimated according to the CML 2001 method (updated in August 2016).



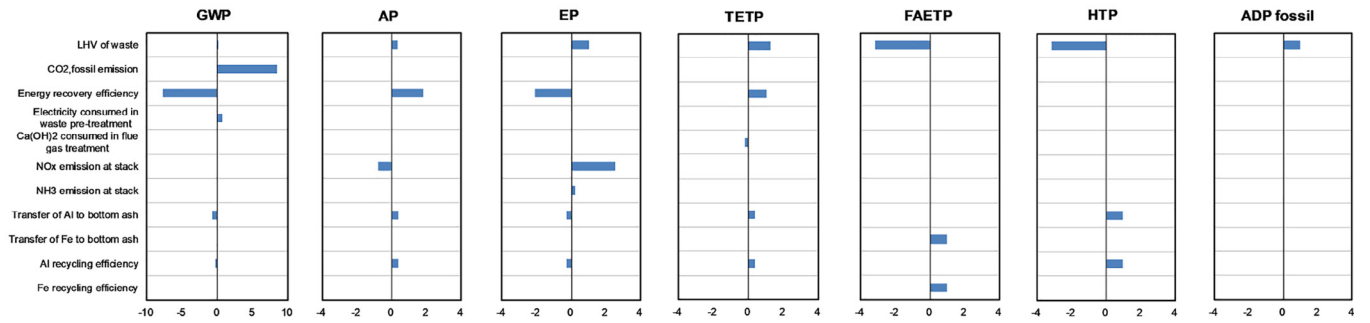
(a) S1: Incineration



(b) S2: Pyrolysis



(c) S3: Gasification



(d) S4: Gasification-melting

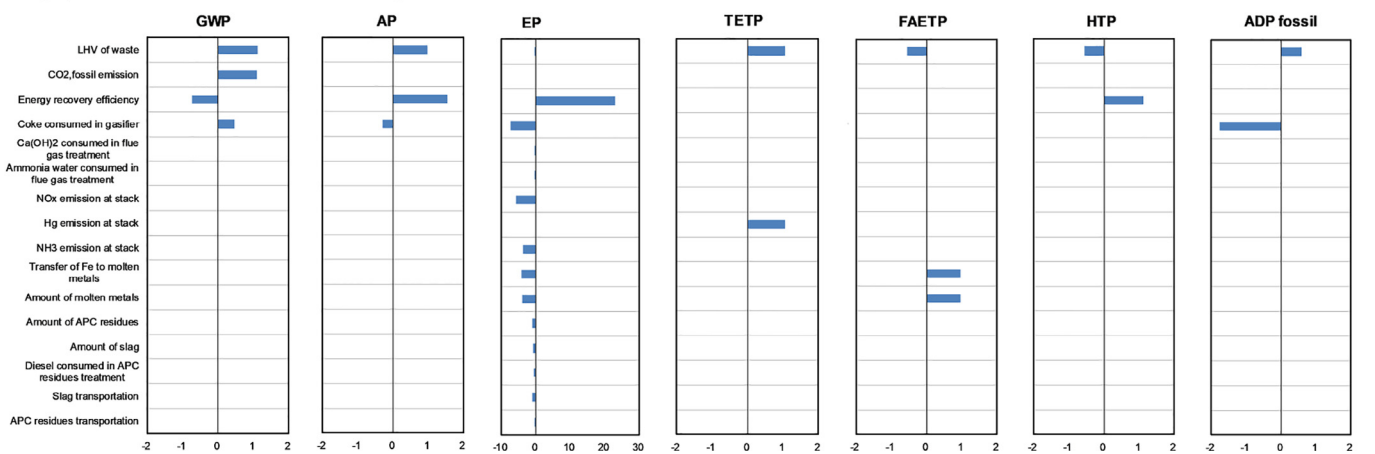


Fig. 5. Perturbation analysis results showing the most important parameters and their sensitivity ratios (SRs) in LCA results of the four different WtE technologies. Only SR greater than 0.2 and SR < -0.2 are presented.

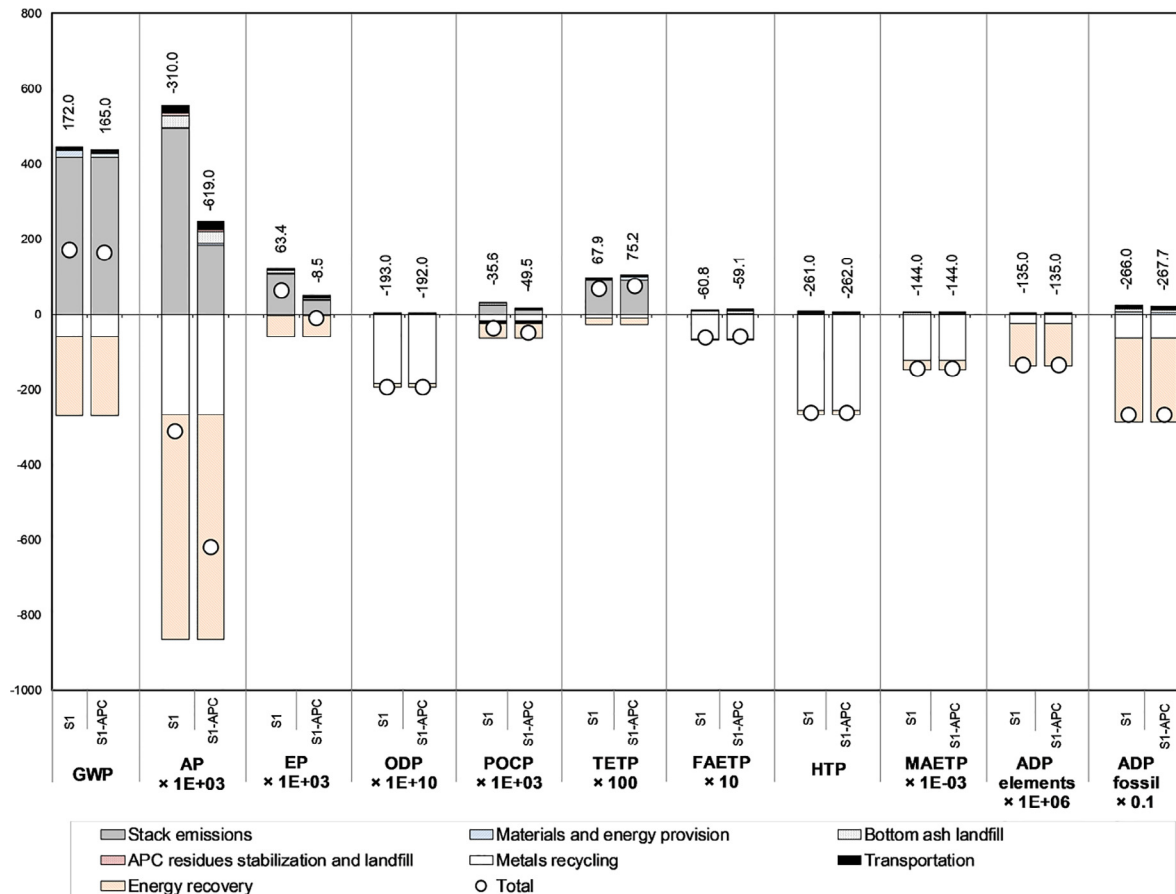


Fig. 6. The effect of improved air pollution control process on the environmental impacts of incineration (S1) WtE technology. Suffix letter “APC” stands for alternative “Air Pollution Control” option. Some impacts are scaled to fit the y-axis; their original values can be obtained by dividing the factor shown on the x-axis.

Table 4

The effect of bottom ash recycling in road construction on the environmental impacts of incineration (S1) and gasification (S3) WtE technologies.

	S1: incineration			S3: gasification		
	S1 (base case)	S1-BA recycling <sup>a</sup>	Variation <sup>b</sup>	S3 (base case)	S3-BA recycling <sup>a</sup>	Variation <sup>b</sup>
GWP [kg CO <sub>2</sub> eq.]	1.72E + 02	1.68E + 02	2.33%	1.04E + 02	1.03E + 02	0.96%
AP [kg SO <sub>2</sub> eq.]	-3.10E-01	-3.43E-01	10.65%	-5.13E-01	-5.26E-01	2.53%
EP [kg Phosphate eq.]	6.34E-02	5.63E-02	11.20%	4.08E-02	3.82E-02	6.37%
ODP [kg R11 eq.]	-1.93E-08	-1.94E-08	0.52%	-1.49E-08	-1.49E-08	0.00%
POCP [kg Ethene eq.]	-3.56E-02	-3.90E-02	9.55%	-4.51E-02	-4.63E-02	2.66%
TETP [kg DCB eq.]	6.79E-01	6.66E-01	1.91%	-2.28E-01	-2.33E-01	2.19%
FAETP [kg DCB eq.]	-6.08E + 00	-6.87E + 00	12.99%	-4.94E + 00	-5.23E + 00	5.87%
HTP [kg DCB eq.]	-2.61E + 02	-2.65E + 02	1.53%	-2.02E + 02	-2.03E + 02	0.50%
MAETP [kg DCB eq.]	-1.44E + 05	-1.47E + 05	2.08%	-1.24E + 05	-1.25E + 05	0.81%
ADP elements [kg Sb eq.]	-1.35E-04	-1.36E-04	0.74%	-1.74E-04	-1.74E-04	0.00%
ADP fossil [MJ]	-2.66E + 03	-2.74E + 03	3.01%	-3.45E + 03	-3.48E + 03	0.87%

<sup>a</sup> Suffix letter “BA recycling” stands for “Bottom Ash recycling” in in specified scenarios.

<sup>b</sup> Grey row named “variation” represents the relative change of environmental impacts in BA recycling case to those in the base case. Only absolute values are presented because all the environmental impacts are decreased in BA recycling case.

SRF, as pre-treatment to upgrade the quality of the incoming waste. For S4 the use of coke appears significant to ADP fossil impact as a consequence of resource use for its production, but also contributes to GWP, AP and EP during its utilization. “Bottom ash landfill” accounts for a greater contribution to FAETP impact in S1 system, to a less extent in S3, due to the consumption of energy for mechanical treatment and the subsequent leaching of heavy metals within the considered time frame. On the other hand, the impacts resulting from “bottom ash landfill” are absent in S2 and S4 scenarios, being substituted by an avoided contribution from “slag recycling”, despite that this benefit is insignificant. As for the rest life cycle stages regarding “transportation”

and “APC residues stabilization and landfill”, they account for an insignificant contribution to all impact categories.

Overall, the contribution analysis has identified key processes contributed to the environmental impacts of each WtE system. Based on the results, a sensitivity analysis is conducted. In the following, the effects of key input parameters, operation conditions, and LCA modelling conditions are separately discussed in Section 3.1, 3.2, and 3.3. Finally, the “best-case” scenarios are discussed in Section 3.4.

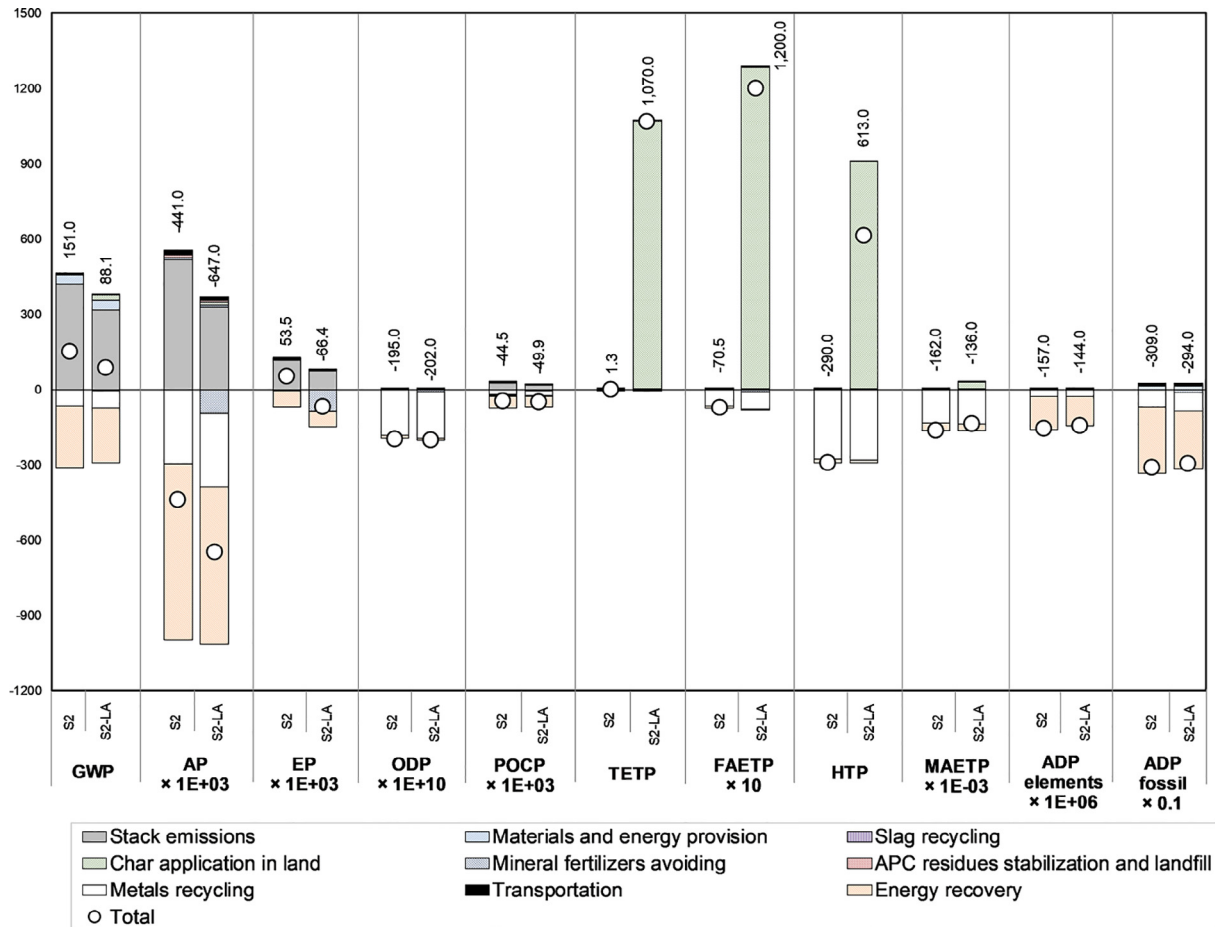


Fig. 7. The effect of applying pyrolysis char in land as soil amendment on the environmental impacts of pyrolysis (S2) WtE technology. Suffix letter “LA” stands for “Land Application” of the pyrolysis char. Some impacts are scaled to fit the y-axis; their original values can be obtained by dividing the factor shown on the x-axis.

### 3.1. Importance of key input parameters to the LCA results

The critical parameters, which significantly affect the LCA results, have been identified through a perturbation analysis. The results are illustrated in Fig. 5 in terms of SR values for seven selected impact categories. The results show that, among the 40–60 input parameters in each WtE system, around 15 parameters have SR values higher than  $\pm 0.2$ . This means that, a 10% change in these parameters would lead to a variation of results larger than 2%.

Energy recovery efficiency is seen to be the most influential parameter for all WtE technologies. The highest SR value of 22.9 is seen for EP of S4. Parameters related to the properties of feedstock, in particular the lower heating value of incoming waste and  $\text{CO}_{2,\text{fossil}}$  stack emission, also stand out in all impact categories. These parameters are mainly dependent on waste composition, which highlight a relatively important role of feedstock variability in determining the total results.  $\text{NO}_x$  stack emission is also an important parameter, and is a result of the waste properties (N content), combustion technology and the effectiveness of APC system. To a lesser extent, Hg and  $\text{NH}_3$  emissions influence TETP and EP, respectively. Other key parameters are mainly related to metals recycling, for example, the amount of metal elements transferred to dedicated fractions (bottom ash in S1 and S3, or char in S2, or molten metals in S4), and their recovery efficiencies. In addition, some parameters are of importance to only specified systems. Examples of such parameters include internal electricity consumption in S2 and S3, and slag and APC residues management in S4. In summary, key parameters determining the environmental performance of WtE technologies are found to be as follows:

- An effective energy recovery is a relatively important parameter, at the same time, efforts should be paid to decrease as much as the internal energy consumption.
- The variation in feedstock plays a crucial role in determining the waste composition (such as, C-fossil and N content) and its heating value.
- An efficient air emissions control system is an important factor, and this is particularly true for  $\text{NO}_x$  removal.
- Metals recycling is also a key parameter and contributes to both non-toxic and toxic impacts.

### 3.2. Importance of operating conditions to the LCA results

#### 3.2.1. Effectiveness of air pollution control

The results from the contribution analysis (Fig. 4) demonstrate a crucial role of stack emissions to final environmental burdens. Due to this reason, the effectiveness of APC process is discussed in this work. In the base case, the APC line in each WtE system is based on “SNCR + dry  $\text{Ca}(\text{OH})_2$  scrubber + activate carbon”. Today, with gradually tightened emission standards, more effective APC techniques have been put in use [50]. As a potential improvement, the use of “wet  $\text{Ca}(\text{OH})_2$  scrubber + activate carbon + SCR” is evaluated. Detailed description of the APC techniques and operating data are provided in the Supplementary Material. Furthermore, the results for incineration case are discussed in Fig. 6. As expected, the related assumptions have led to a better environmental performance in S1-APC scenario, particularly in terms of AP, EP and POCP, which show a decrease of 99%, 113% and 39% as compare to S1, respectively. Compared to the results presented in Fig. 3, it is observed that AP, EP and POCP impacts of S1-APC

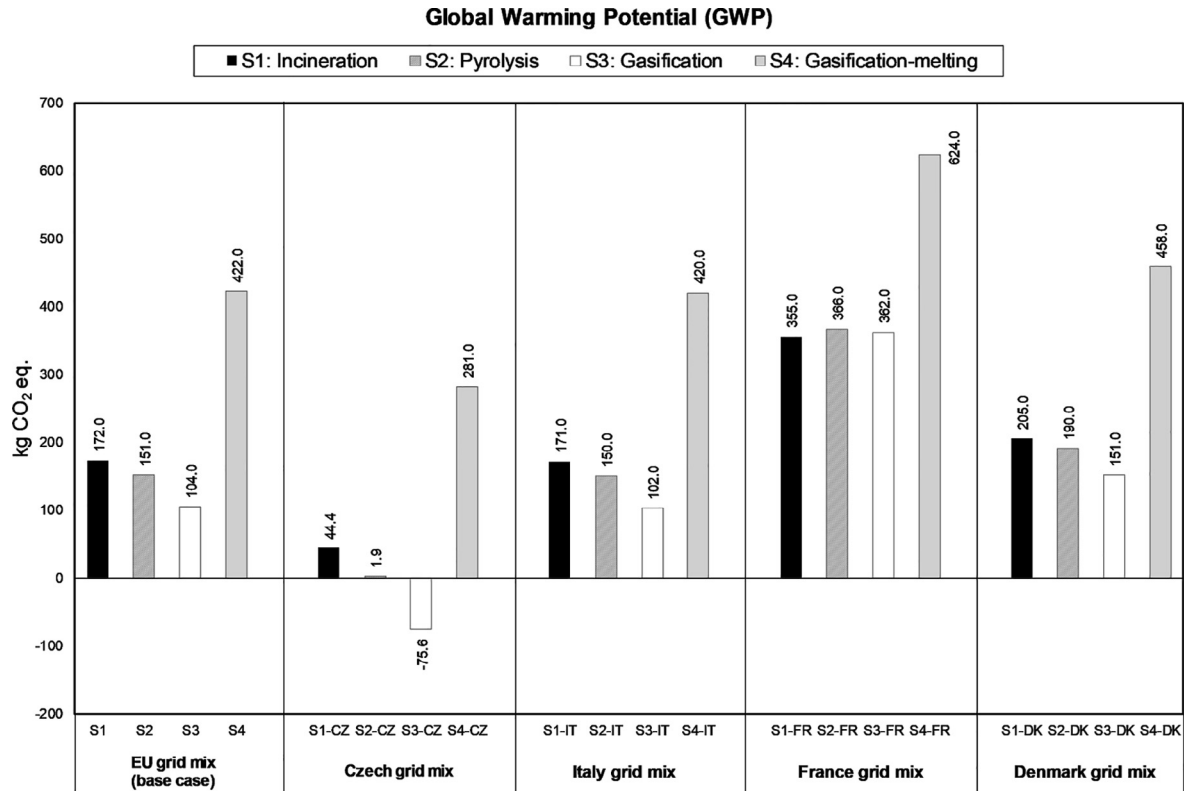


Fig. 8. The effect of substituted options for electricity generation on the global warming potential (GWP) of the four different WtE technologies.

scenario have surpassed pyrolysis and gasification scenarios (S2-S4) and become the most environmental-friendly scenario. As indicated previously in Fig. 5, this benefit is mainly due to the decreased  $\text{NO}_x$  emission, and to a lesser extent, due to the decreased  $\text{SO}_2$ , HCl and  $\text{NH}_3$  emissions.

Based upon this analysis, implementation of a more effective APC process can significantly reduce the overall environmental impacts, thus determining the relative sustainability of different WtE systems.

### 3.2.2. Bottom ash recycling

The results shown in Fig. 4 indicate varied environmental impacts from “bottom ash landfill” (in S1 and S3) and “slag recycling” (in S2 and S4) processes. The former is seen as an environmental burden due to the consumption of energy in landfill operation and leaching of toxic substances. Realizing that bottom ash shows similar technical properties to those of natural aggregates, increasing efforts are taken to utilize bottom ash in road construction in many EU countries [51,52]. For this reason, the “bottom ash recycling” case is assessed in this work. Key data used for model estimation are detailed in the Supplementary Material, and the results are presented in Table 4.

Compared with the base case, assumptions on bottom ash recycling have resulted in decreased impacts for all categories. The benefits are mainly derived from the following factors: (1) decrease in energy consumption associated with ash landfill, (2) reduction in the provision of natural gravel. Incineration (S1-BA recycling) generally shows more sustainable impacts than gasification (S3-BA recycling), which is due to a higher amount of bottom ash generated and being recycled. However, the results show that the effect of bottom ash recycling is quite marginal, which does not change the overall ranking of different WtE systems. Similar findings were drawn by Birgisdottir [53], who report fairly equal environmental impacts for recycling or landfill of incineration bottom ash. The results on the other hand indicate that recycling can serve as a potential future management option for bottom ash, which in fact would be preferred over landfill as a means for

conserving resources. For this option, the limitation lies within the leaching emissions, as has recently been assessed by Allegrini [21] that road application of bottom ash may potentially lead to higher release of toxic substances.

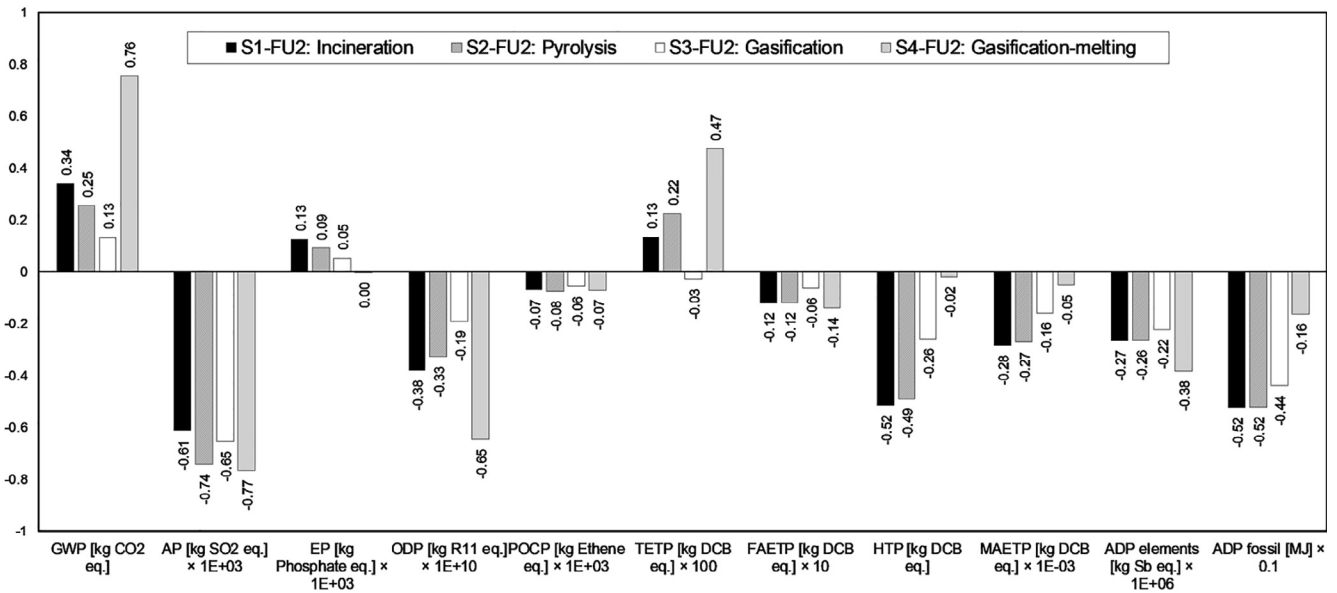
### 3.2.3. Pyrolysis char utilization in land application

In the base case, char generated from pyrolysis is used as an energy source for electricity recovery. Comparatively, char applied in land is considered in this work. The LCA boundary of the char application process consists of char transport to dedicated farms, spreading it on soil, and the subsequent effects to soil. While energy utilization of char in the base case avoids electricity production, the land application of char provides several merits, including substitution of mineral fertilizers (N, P and K), and long-term carbon sequestration. Detailed calculation is available in the Supplementary Material.

Fig. 7 shows the associated environmental impacts along with those from the base case. Char utilization in land shows higher saved impacts regarding GWP, AP and EP, and to lesser extent for ODP and POCP. Looking at the contribution of each life cycle stage, majority of the reduced impacts are associated with the decreased stack emissions, which is due to the exempted char combustion. The benefit is also reflected by a negative contribution from the avoided production of mineral fertilizers, particularly for AP and EP. Conversely, the land application case significantly increases toxic impacts, such as TETP, FATEP and HTP, which is mainly due to metal emissions, and originally contained in char yet transferred to soil.

In short, the utilization pathway of pyrolysis char would greatly influence the environmental performance of pyrolysis (S2) system. Overall, it is difficult to figure out which application option is more favourable. However, critical life cycle hotspots can be identified. For example, it is important to consider the potential risk of metal contaminants if char is to be used in land. This requires efforts to reduce the concentrations of metals in char, or modify them to become less reactive. Overall, there is a need to carefully address the potential

(a) Environmental impacts, with reference to the functional unit of 1kwh of electricity generated



(b) Environmental impacts, with reference to the functional unit of 1kwh of exergy in output products

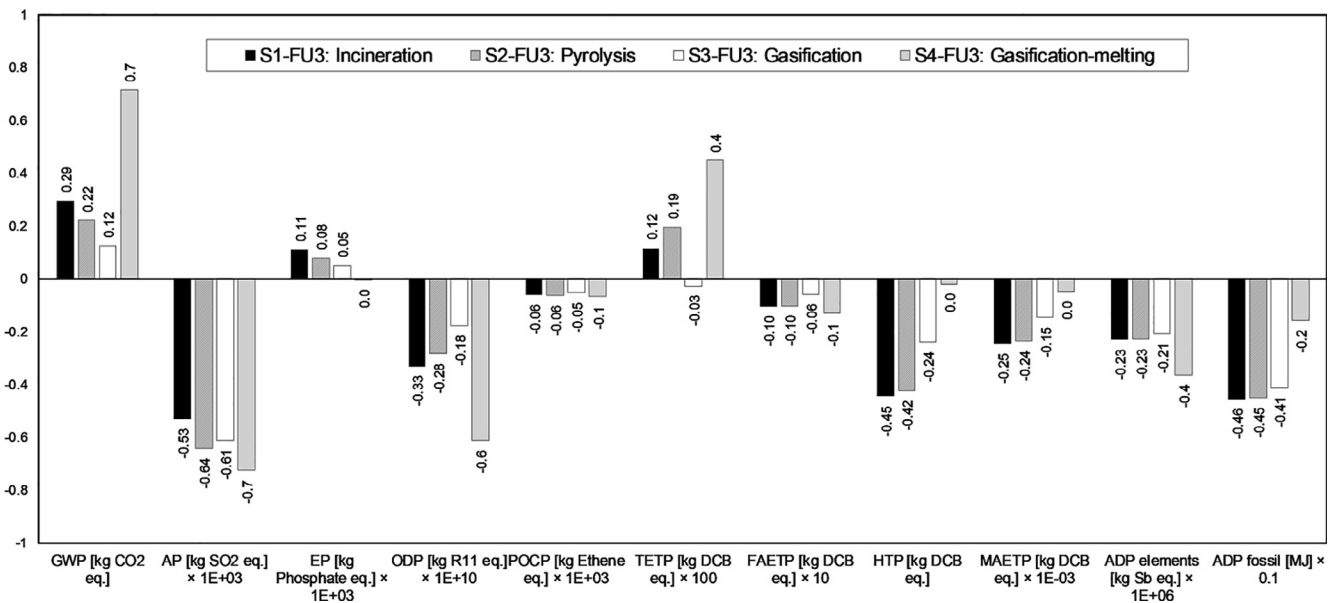


Fig. 9. The effect of using alternative functional unit on the environmental impacts of the four different WtE technologies: (a) with reference to 1 kwh of electricity generated; (b) with reference to 1 kwh of exergy in output products. Some impacts are scaled to fit the y-axis; their original values can be obtained by dividing the factor shown on the x-axis.

burdening impacts, so as to properly determine a better utilization route for char.

### 3.3. Importance of model conditions to the LCA results

#### 3.3.1. Substituted energy sources

In the base case, the electricity produced is assumed to substitute the one provided by the EU grid mix. Concerning the importance of energy recovery process, alternative energy sources in individual countries are considered as substituted options, and these countries include Czech, Italy, France, and Denmark. These countries are selected because electricity from Czech is “dirtier” based on higher utilization of coal (50.4%). The French and Italian grid mixes are instead “cleaner” due to a predominant role of respectively nuclear (72.5%) and natural gas (44.5%) in their energy infrastructures. However, a higher ratio of

renewables (60.5%) is observed for Denmark’s energy infrastructure [28].

The results for GWP impact are shown in Fig. 8. It is noted that the sources of substituted electricity heavily affects the LCA results. GWP under different substituted energy sources is found to be in the following descending order: France > Denmark > EU grid mix > Italy > Czech. This is due to the reason that, more the electricity is produced based on fossil fuels, higher are the GWP emissions, thus allowing increased environmental credits. The overall ranking of WtE systems changes, which means that GWP from incineration (S1) outperforms gasification (S3), provided the displaced electricity is based on French grid mix. This can be explained by the higher amount of electricity recovered from S3, which is more sensitive to the source of energy to be substituted.

These results are in accordance with the previous findings

**Table 5**  
The effect of using alternative long-term time frame (60,000 years) on the environmental impacts of incineration (S1) and gasification (S3) WtE technologies.

	GWP [kg CO <sub>2</sub> eq.]	AP [kg SO <sub>2</sub> eq.]	EP [kg Phosphate eq.]	ODP [kg R11 eq.]	POCP [kg Ethene eq.]	TETP [kg DCB eq.]	FAETP [kg DCB eq.]	HTP [kg DCB eq.]	MAETP [kg DCB eq.]	ADP elements [kg Sb eq.]	ADP fossil [MJ]
Base case (100 years)											
S1	1.72E + 02	-3.10E-01	6.34E-02	-1.93E-08	-3.56E-02	6.79E-01	-6.08E + 00	-2.61E + 02	-1.44E + 05	-1.35E-04	-2.66E + 03
S3	1.04E + 02	-5.13E-01	4.08E-02	-1.49E-08	-4.51E-02	-2.28E-01	-4.94E + 00	-2.02E + 02	-1.24E + 05	-1.74E-04	-3.45E + 03
Long-term time frame											
S1-LT <sup>a</sup>	1.72E + 02	-3.10E-01	6.35E-02	-1.93E-08	-3.56E-02	6.87E-01	3.19E + 02	-2.59E + 02	-7.96E + 04	-1.35E-04	-2.66E + 03
S3-LT <sup>a</sup>	1.04E + 02	-5.13E-01	4.57E-02	-1.49E-08	-4.51E-02	-2.28E-01	1.30E + 02	-2.01E + 02	-9.69E + 04	-1.74E-04	-3.45E + 03

Legend with dark grey indicates a high changing of the impacts, light grey low and white with no changing.  
<sup>a</sup> Suffix letter "LT" stands for "Long-Term" time frame in specified scenarios.

[9,54,55]. The results highlight that, the assumptions on the substituted energy should be adequately addressed. For example, the geographical location of the specified plant has a certain significance, especially when the aim is to select an environmentally optimal WtE technology.

### 3.3.2. Alternative functional units

The robustness of LCA results is tested by changing the perspectives of functional unit. The "input-oriented" functional unit in the base case (i.e. 1 tonne of MSW) is shifted to two alternative "output-oriented" ones, as follows: (1) 1 kwh of electricity generated, and (2) 1 kwh of exergy in the output products. The calculation data are provided in the [Supplementary Material](#).

[Fig. 9](#) shows generally decreased impacts across all categories, which are 2–3 orders of magnitude less than the base case. This is expected, as from the input-oriented perspective, the treatment of 1 tonne of MSW can result in around 500–800 kwh of electricity generation. Changing the functional unit has altered the ranking of different scenarios. An improved performance is observed for incineration (S1-FU2, S1-FU3) regarding HTP, MAETP and ADP fossil impacts, and gasification-melting (S4-FU2, S4-FU3) regarding AP and POCP impacts. This can be explained by the differences of energy efficiencies. Gasification (S3) and pyrolysis (S2) produce higher amount of electricity and exhibit greater avoided (negative) impacts from the input-oriented perspective. However, this benefit is offset if the functional unit is fixed at an identical amount of electricity or exergy output. The results also show that the delivery of 1 kwh of electricity ([Fig. 9a](#)) or 1 kwh of exergy ([Fig. 9b](#)) has little difference in environmental impacts, which is due to the reason that exergy contained in the recovered electricity has contributed to a majority proportion (87–95%) of the total output products. Overall, this analysis confirms that changing the functional unit in LCA would result in different environmental performance. The comparison of different WtE systems requires a very cautious selection of input or output perspective in order to properly interpret the results.

### 3.3.3. Long-term time frame

The time frame considered in this study is 100 years, which follows the common practice observed within the LCA. However, it is necessary for the sensitivity analysis to consider a long-term time frame, which aims at quantifying the "worst case" environmental consequences.

The analysis is focused on bottom ash after it is landfilled, and therefore, is relevant only for incineration (S1) and gasification (S3) systems. The long-term perspective considers 60,000 years, using TCs of substance leaching sourced from Doka [23]. The resulted environmental impacts are listed in [Table 5](#). As expected, increased burdens are shown when expanding the time frame. This affects mainly the toxic-related impacts, together with EP, which are ascribed to accumulated leaching of heavy metals. Among all categories, FAETP and MAETP are considerably more sensitive, particularly FAETP impact is shifted from an environmental saving to a burden, which has significantly deteriorated the performance of incineration and gasification cases.

### 3.4. "Best-case" scenarios

Finally, two "best-case" scenarios are modelled. The aim is to examine the performance of most state-of-the-art WtE technologies.

For incineration (S1), the operating data from AEB plant in Amsterdam are analysed [44]. Due to innovative optimizations, such as increasing steam parameters (440 °C, 125 bar), use of steam reheating and water-steam cycle, and flue gas recirculation, the net energy efficiency of the plant reaches 30.6%, which is the highest among world's incineration plants. The APC employs "SNCR + activate carbon + wet Ca(OH)<sub>2</sub> scrubber" to control stack emissions (see details in the [Supplementary Material](#)). The plant also recycles various residual materials. The results shown in [Fig. 10](#) confirm an improved environmental performance from the use of this Best Available Technology (BAT). All impacts from SI-BAT case show 4–229% decrease compared

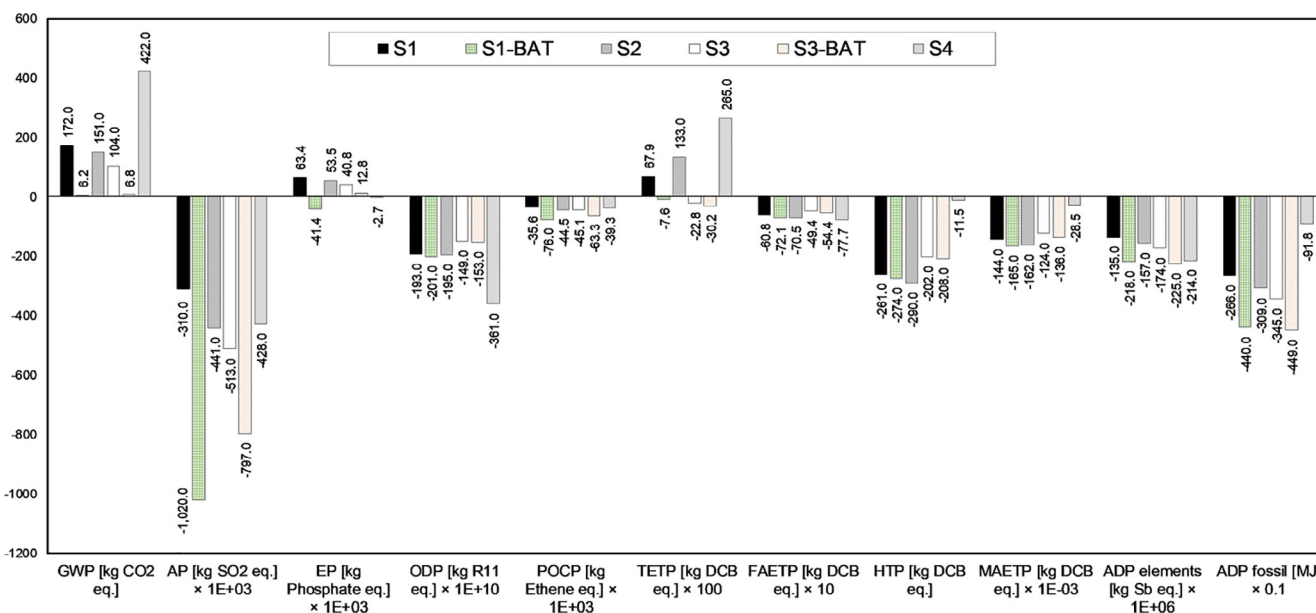


Fig. 10. The effect of using Best Available Technology in incineration (S1) and gasification (S3) WtE technologies. Suffix letter “BAT” stands for “Best Available Technology”. Some impacts are scaled to fit the y-axis; their original values can be obtained by dividing the factor shown on the x-axis.

to the base case (S1). The S1-BAT case has effectively surpassed S2, S3 and S4, showing the lowest impacts regarding 6 out of 11 categories (GWP, AP, EP, POCP, MAETP and ADP elements). This reveals that modern incineration has the potential to fulfill an environmentally sound technology, over pyrolysis and gasification at present.

For gasification (S3), the “best-case” scenario is not dedicated to examining the performance of an alternative plant. Instead, the potential of the co-firing of cleaned syngas in existing boilers is assessed. This option represents one of the future perspectives for gasification due to several reasons [56,57]: (1) cleaned syngas connected to for example a coal-fired boiler allows the use of high steam parameters, thus exhibiting a huge potential to improve energy recovery efficiency; (2) the introduction of gas instead of solid fuels into boilers can minimize problems related to correction, fouling, and ash quality; (3) the utilization of existing infrastructure can reduce the requirements for additional investment. For these purposes, S3-BAT scenario considers that the syngas produced from gasification is sent for co-firing in a coal plant, and assumes a net electricity efficiency of 35.4% based on the value of EU average [58]. The results presented in Fig. 10 show that S3-BAT scenario provides a superior performance with regards to 6 out of 11 impacts (GWP, AP, POCP, TETP, ADP elements and ADP fossil) when compared with the four WtE base cases. This again verifies the importance of boosting energy efficiency.

#### 4. Discussion and future recommendations

The comparison among four most common WtE technologies, namely incineration (S1), pyrolysis (S2), gasification (S3), and gasification coupled with ash melting (S4), indicates an overall sustainable performance of all considered systems, which means that 8 out of 11 impacts show net environmental benefits. The impacts are much lower than those from the EU grid mix. For example, for the generation of 1 kWh of electricity, WtE technologies have the potential to reduce 18–68% of GWP (except for S4) by avoiding coal and natural gas. A brief calculation is conducted from a much broader perspective of functional unit, and assumes that the WtE plants are dedicated to managing 2,000 t/d of residual waste, which is a typical treatment capacity by a good sized metropolitan city [59]. In such a case, 23,000–130,000 tonnes of GWP emissions per year could be avoided from the EU grid mix, which are equivalent to 16,000–25,000 tonnes of

coal and 12–19 million m<sup>3</sup> of natural gas. This fact clearly indicates the huge potential for future development of WtE technologies.

The results from both contribution analysis (Fig. 4) and perturbation analysis (Fig. 5) confirm that energy recovery efficiency is one of the most critical parameters affecting the environmental performance of WtE technologies. The results presented in Fig. 10 further reveal the importance of improving plant efficiency in determining the relative ranking of each technology. This clearly indicates potential future areas for development. For incineration, positive experience gained from Amsterdam’s AEB plant could serve as the basis of a number of technical optimisations designed to improve energy efficiency. For pyrolysis and gasification, a feasible application would be the use of syngas in existing power stations or other industrial plants, where the process could benefit from higher efficiency of host plants. Potential long-term development of pyrolysis and gasification includes the use of more efficient equipment, such as a combined cycle gas turbine [60]. However, this application has not yet matured enough to meet the market demand.

The results from this study show developing attractiveness for pyrolysis and gasification WtE technologies. However, these technologies are still less commercialized at present. One important obstacle is associated with the variability of feedstock, as the applications of pyrolysis and gasification to WtE are often limited to few specific waste fractions (such as, SRF, plastic, and rubber tyres [61]). Factually, a higher degree of pre-treatment is generally required, even if some gasification technologies are able to accept raw MSW (for example, S4 system in this study). Therefore, improving the fuel quality seems important to reduce as much as of energy consumed for waste segregation, drying, and homogenization. A feasible approach could be to integrate the plants with an upstream material recovery facility, or mechanical biological treatment plants. Besides, waste pre-processing before WtE is also efficient for incineration, as is shown in Fig. 5, increasing the waste lower heating value enables a higher recovery of electricity to effectively decrease the associated environmental burdens.

Energy, environment, economic, and social performance of WtE technologies are all of great interest to authorities [2,62]. Therefore, a brief discussion of economic aspect is conducted in this work. It is evident that an accurate cost estimation and fair comparison among different WtE technologies cannot be addressed. This is due to a variety of issues, such as: (i) lack of sufficient operational data; (ii) variations in

regional energy cost, availability of resources; (iii) variations in governmental regulations and incentives [3]. Despite this fact, a detailed literature review of the cost structure of WtE technologies shows comparable annual capital and net operational cost between incineration and pyrolysis/gasification [63]. Several studies [64,65] have shown that the net cost from gasification plants can even be lower than that from incineration, which is due to the higher efficiency of gasification that allows for a higher revenue from the export of electricity. Apart from these spatial and temporal factors, scale effects should also be accounted for when different WtE options are compared. This is due to the reason that an increasing plant size can lead to a drop in treatment cost [3].

To conclude, a range of critical input parameters, processes, operating conditions and modelling assumptions influence the environmental impacts of different WtE technologies and have been identified comprehensively in this study. These factors should therefore be focused on when considering potential areas of improvements throughout all stages of each WtE technology.

### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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### Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.enconman.2019.06.016>.

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