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A new transient thermal fouling probe for cross flow tubular heat exchangers

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A B S T R A C T

The present probe is developed in order to accurately estimate in situ not only the convective exchange coefficient but also the fouling thickness of heat exchangers from a reliable transient state estimation method. The originality of the estimation method consists in considering a global response time of the system in fouling conditions to be compared to clean conditions. The sensitivity function is then built from the experimental signal without precise knowledge about the model or the absolute thermophysical properties. The reliability of the method is demonstrated in theoretical cases and with calibrated experiments.

Keywords:

Particulate fouling

Tubular heat exchangers

Thermal sensor

Transient method

Weighted sum of transient data

Parameters estimation

1. Introduction

Heat exchangers are used in numerous industrial processes. They can also be found as part of many systems in transportation and residential and tertiary applications. Most heat transfer operations involve the deposition of unwanted residues on exchange surfaces. In gaseous systems, the deposition of particulate matter constitutes the fouling. The effectiveness of heat exchangers can decrease because of this foulant deposition onto the heat transfer surface. Attempts have been made to model heat exchangers fouling. Pioneer work [6,16], essentially an asymptotic curve-fitting exercise, tends to dominate the concepts and leaves much to empiricism. Marner [9] reviewed several analytical and experimental studies relating developments in gas side fouling. Other models [1–4,13,18,19] are based on deposition and removal mechanisms, but they still involve a strong empirical content.

Ever since the end of the 1970s, some gas-side fouling measuring devices have been envisaged [5,7,10–12,14,17]. All of them provide physical information on fouling. Nevertheless, they are still far from giving thermal information and taking into account the deposit phenomena involved.

Thus, although considerable work has been carried out through the years, it is clear that progresses remain to be made, more particularly to provide the basis for improved predictive methods. Currently, the various solutions, even if they are numerous and varied, are not completely satisfactory. However, they allowed to work out the main quality that a fouling probe has to present. In particular, it has to be cheap, easy to implement and it has to take into account the heat transfer and the deposit phenomena involved [20].

So, the here developed probe replaces directly a part (or the totality) of the tubular heat exchanger. This device can be described by a multilayered system where the transient temperature measurement is achieved simultaneously and at the same location as a thermal excitation. The associated data processing is developed in order to estimate the heat transfer coefficient and the particulate fouling thickness of tubular heat exchanger. Indeed, such parameters enable to determine heat exchangers fouling level.

The 3D transient heat transfer problem is modelled by an extension of the thermal quadrupole formalism. The study of the transfer function linking excitation to system temperature response allows the probe sizing and the theoretical sensitivity study establishment.

Since the probe must be used in harsh conditions, since the nominal values of the problem are not precisely known, the estimation method is directly realised from the experimental temperature responses. This method is sturdy and is based on an experimental sensitivity study. It does not require sophisticated physical considerations or complete forward model. So, two simplified transient forward models have been developed.

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Nomenclature

Latin letters

A, B, C, D	quadrupole coefficients
C_p	constant pressure specific heat ($\text{J kg}^{-1} \text{K}^{-1}$)
L	heater half length (m)
M	quadrupole matrix
M_{-1}	-1 order moment (K)
N	acquisition points
Q	flowrate ($\text{m}^3 \text{s}^{-1}$)
R	resistance ($\text{W}^{-1} \text{K}$)
S	area (m^2)
T	temperature (K)
X	sensitivity coefficient
a	thermal diffusivity ($\text{m}^2 \text{s}^{-1}$)
b	heater width (m)
e	thickness (m)
h	convective heat transfer coefficient ($\text{W m}^{-2} \text{K}^{-1}$)
k	Fourier coefficient
p	Laplace variable (s^{-1})
r	radial coordinate (m)
t	time (s)
x	angular coordinate (rad)

z axial coordinate (m)

Greek letters

α_n	Fourier variable
β	parameters vector
ϕ	radial heat flux (W)
φ	heat flux produced by the heater (W)
λ	thermal conductivity ($\text{W m}^{-1} \text{K}^{-1}$)
ρ	density (kg m^{-3})
σ^2	standard deviation
θ	Laplace transform of T
τ	characteristic time constant (s^{-1})

Symbols

$-$	normalized
\sim	Fourier transform
$*$	reduced

Subscripts

c	clean
d	deposit

A testing bench has been realised in which the probe is laid out to obtain experimental results in clean or in fouling conditions.

At first, the probe description is realised. Then, the different transient forward models are developed and the theoretical sensitivity analysis from the 3D forward model is presented. Lastly, experimental data in clean and in fouling conditions are detailed and the estimation method is presented and validated.

2. Probe description

The studied probe, 50 mm length, 5 mm inside radius and 13 mm outside radius, can be described by a cylindrical multilayered system (Fig. 1). Each layer is 2 mm thick. The internal and the external layers are in stainless steel to be able to come under the same thermohydraulic and fouling influences as exchangers. A copper slab (10 mm length, 2/10 mm thick) heated by Joule effect produced by a heat step, encircling the centre section of the cylinder and is inserted between two other layers. These layers are in polytetrafluoroethylene polymer (PTFE) to be able to limit heat transfer from the heater and to make insignificant the contact resistances. The power supply to the heating element is controlled through a constant-voltage transformer. The final constituted pipe is inserted between two stainless steel tubes which act as heat exchangers parts. The temperature variation along the heater is measured by several T type thermocouples implanted parallel to the cylinder axis.

3. Experimental device

The probe is inserted into a testing bench named GAZPAR (GAZ PARTICLES) to be both tested in clean conditions and in fouling conditions. It is a three parts system (Fig. 2). The probe is mounted in a rectangular wind tunnel with $80 \times 80 \text{ mm}^2$ a cross section. The fluid used is air at 323 K. A flow of cool water is sent through the central stainless steel pipe to simulate real tubular heat exchangers conditions and to maintain the probe inlet surface temperature at a constant value.

The probe then acts as a foulant deposition site by simulating a heat exchanger tube in the gas stream. The primary constituents in exhaust gases causing fouling include SiO_2 , Na_2SO_4 , and CaSO_4 [16]. So, fouling tests were carried out using sodium sulfate of 4 μm medium diameter in the gas stream as foulant. The foulant

particles are generated by ultrasound pulverization. Such generator achieves a particle size distribution close to monodispersity.

4. Forward models

The thermal quadrupole formalism using integral transforms methods [8] is used to model the three-dimensional transient heat transfer in the studied multilayered system. The interest of this approach lies in the fact that a linear relationship is given between the input and the output temperature and the heat flux after a double Laplace Fourier transform. The main advantage of this temperature-flux vector representation is to make the analytical modelling of multimaterials possible by multiplying the corresponding quadrupole matrices.

4.1. 3D forward model

The following case (Fig. 3) where the transient temperature measurement is achieved simultaneously and at the same location as a thermal excitation carried out by the heater is considered.

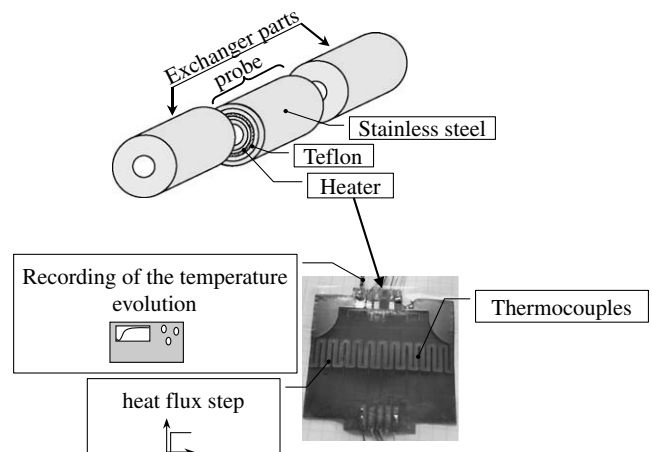


Fig. 1. Schematic diagram of heat transfer probe.

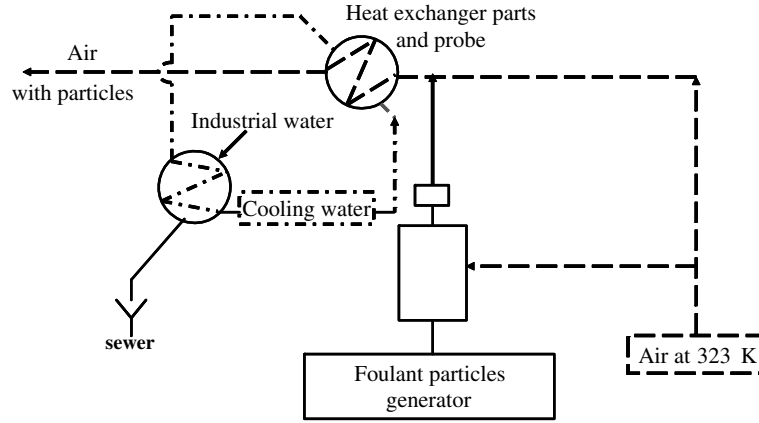


Fig. 2. Experimental device scheme GAZPAR.

In this model, the axial and radial and angular conductions into each layer and between the layers, the contact resistance between each layer and the probe inertia are considered. The three-dimensional transient heat transfer in the multilayered system supposes that the thermal properties are assumed to be constant during the experiment. The probe is initially at thermal equilibrium.

The temperature $T(r, z, x, t)$ at the level of the heater is the solution of the following heat equation in cylindrical coordinates:

$$\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T(r, z, x, t)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T(r, z, x, t)}{\partial x^2} + \frac{\partial^2 T(r, z, x, t)}{\partial z^2} = \frac{1}{a} \frac{\partial T(r, z, x, t)}{\partial t} \quad (1)$$

where a is the thermal diffusivity, r is the radial coordinate, z is the axial coordinate and x is the angular coordinate.

To solve the heat equation through an analytical way, it is convenient to consider the following boundary conditions of the problem:

$$r = r_7 - \lambda(2\pi r_7) \frac{\partial T(r_7, z, x, t)}{\partial r} = h(r, x)(2\pi r_7) T(r_7, z, x, t) \quad (2)$$

$$z = L \quad T(r, L, x, t) = 0 \quad (3)$$

where $h(r, x)$ is the convective heat transfer coefficient.

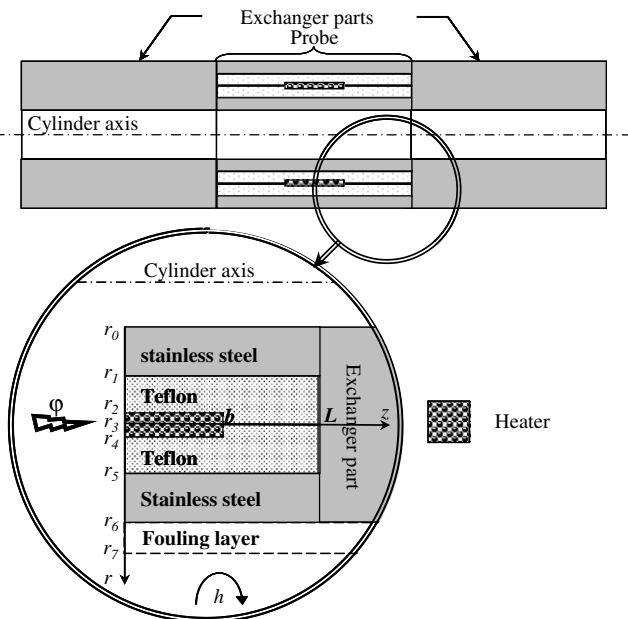


Fig. 3. Schematic representation of theoretical model.

Such condition (3) is a suitable approximation since the metallic sample in contact with the system at this boundary is very effusive. Such assumption has been verified with numerical simulation [22].

$$r = r_3 \begin{cases} \phi(r_3^+, z, x, t) = \phi(r_3^-, z, x, t) + \phi H(t) & \text{if } 0 < z < b \\ \phi(r_3^+, z, x, t) = \phi(r_3^-, z, x, t) & \text{when } 0 < z < L \end{cases} \quad (4)$$

where $H(t)$ is the Heaviside function and ϕ is the heat flux produced in the heater.

The cooling water flowing through the inner cylinder sets its own temperature:

$$r = r_0 \quad T(r_0, z, x, t) = 0 \quad (5)$$

The problem is considered as symmetric with respect to the plane $x = 0$ and $z = 0$. Indeed, the whirling frequency downstream the cylinder is up to 40 Hz in the considered operating conditions (air flow rate of $100 \text{ Nm}^3 \text{ h}^{-1}$). Thus, the wake effect can be neglected:

$$z = 0 \quad \frac{\partial T(r, 0, x, t)}{\partial z} = 0 \quad (6)$$

$$x = 0 \quad \frac{\partial T(r, z, 0, t)}{\partial x} = 0 \quad (7)$$

$$x = \pi \quad \frac{\partial T(r, z, \pi, t)}{\partial x} = 0 \quad (8)$$

The initial condition is:

$$t = 0 \quad T(r, x, z, t = 0) = 0 \quad (9)$$

The periodicity conditions to the x -coordinate and the symmetry conditions relative to the z -coordinate enable to use the Fourier cosine transform of the temperature and of the flux in the x - and z -direction associated with a Laplace transform applied to the time variable:

$$\tilde{\theta}(r, \alpha_n, k, p) = \int_0^\infty \int_0^L \int_0^\pi T(r, z, x, t) \cos(\alpha_n z) \times \cos(kx) e^{-pt} dx dz dt \quad \text{with} \quad \alpha_n = \frac{(n + \frac{1}{2})\pi}{L} \quad (10)$$

where $\tilde{\theta}(r, \alpha_n, k, p)$ is the Laplace Fourier transform of the temperature $T(r, x, z, t)$.

Note that if the symmetry condition to the x -coordinate is not achieved, it would be more appropriate to consider complex Fourier transform to take into account the x -coordinate periodicity between $x = 0$ and $x = 2\pi$.

So, the heat equation becomes in transformed space:

$$\frac{1}{r} \frac{d}{dr} \left(r \frac{d\tilde{\theta}(r, \alpha_n, k, p)}{dr} \right) = \left(\frac{p}{a} + \alpha_n^2 + \frac{k^2}{r^2} \right) \tilde{\theta}(r, \alpha_n, k, p) \quad (11)$$

Eq. (11) admits for general solution:

$$\tilde{\theta}(r, \alpha_n, k, p) = C_1 I_k \left(\sqrt{\frac{p}{a} + \alpha_n^2} r \right) + C_2 K_k \left(\sqrt{\frac{p}{a} + \alpha_n^2} r \right) \quad (12)$$

where C_1 and C_2 are the integration constants and where I_k and K_k represent, respectively, the modified Bessel functions of the first kind and of the second kind.

The transformed expression of the boundary condition (4) yields:

$$\tilde{\phi}(r_3^+, \alpha_n, k, p) = \tilde{\phi}(r_3^-, \alpha_n, k, p) + \frac{\varphi}{p} \frac{\sin(\alpha_n b)}{\alpha_n} \frac{\sin(kx)}{k} \quad (13)$$

Expressions (11) and (13) are then equivalent to a quadrupole presentation. So, the following matrix relationship between the Laplace–Fourier temperature-flux vectors can be written using this quadrupole formalism for a cylindrical layer $r_{\text{out}} - r_{\text{in}}$ thick limited by two cylindrical surfaces of radii $r = r_{\text{in}}$ and $r = r_{\text{out}}$:

$$\begin{bmatrix} \tilde{\theta}(r, \alpha_n, k, p) \\ \tilde{\phi}(r, \alpha_n, k, p) \end{bmatrix}_{r_{\text{in}}} = M \begin{bmatrix} \tilde{\theta}(r, \alpha_n, k, p) \\ \tilde{\phi}(r, \alpha_n, k, p) \end{bmatrix}_{r_{\text{out}}} \quad (14)$$

$$= \begin{bmatrix} A & B \\ C & D \end{bmatrix}_{r_{\text{in}}, r_{\text{out}}} \begin{bmatrix} \tilde{\theta}(r, \alpha_n, k, p) \\ \tilde{\phi}(r, \alpha_n, k, p) \end{bmatrix}_{r_{\text{out}}}$$

with the following values of the coefficients A, B, C, D of the quadrupole matrix defined as:

$$\left. \begin{aligned} A &= \gamma r_{\text{out}} [I_k(\gamma r_{\text{in}}) K_{k+1}(\gamma r_{\text{out}}) + I_{k+1}(\gamma r_{\text{out}}) K_k(\gamma r_{\text{in}})] \\ B &= \frac{1}{\pi \lambda} [I_k(\gamma r_{\text{out}}) K_k(\gamma r_{\text{in}}) - I_k(\gamma r_{\text{in}}) K_k(\gamma r_{\text{out}})] \\ C &= \pi \lambda r_{\text{in}} r_{\text{out}} \gamma^2 [I_{k+1}(\gamma r_{\text{out}}) K_{k+1}(\gamma r_{\text{in}}) - I_{k+1}(\gamma r_{\text{in}}) K_{k+1}(\gamma r_{\text{out}})] \\ D &= \gamma r_{\text{in}} [I_k(\gamma r_{\text{out}}) K_{k+1}(\gamma r_{\text{in}}) + I_{k+1}(\gamma r_{\text{in}}) K_k(\gamma r_{\text{out}})] \end{aligned} \right\} \quad (15)$$

with $\gamma = \sqrt{\frac{p}{a} + \alpha_n^2}$

Each layer can now be described by its own quadrupole and the multilayered system can be modelled by multiplying the corresponding quadrupole matrix.

Finally, the temperature at the level of the heater in the Laplace–Fourier space can be written as:

$$\tilde{\theta}(r_3, \alpha_n, k, p) = \left[\frac{C_1 + D_1 h (2\pi r_7)}{A_1 + B_1 h (2\pi r_7)} + \frac{A_2}{B_2} \right]^{-1} \frac{\varphi}{p} \frac{\sin(\alpha_n b)}{\alpha_n} \frac{\sin(kx)}{k} \quad (16)$$

To return to the Laplace space, the appropriate inverse Fourier transform (17) is used:

$$\theta(r_3, x, z, p) = \frac{2}{L} \sum_{n=0}^N \tilde{\theta}(r_3, \alpha_n, p) \cos(\alpha_n z) \quad (17)$$

To return to the real time space, the Gaver–Stehfest numerical algorithm [15] is used.

At this stage, this model has too many approximations hard to check. Physical phenomena complexity (boundaries conditions validity, concept of heat transfer coefficient in transient state...) compared with industrial conditions (measurement noise...) does not allow to use the previous model to estimate accurately, in a classical manner, the heat transfer coefficient and the density variation of the fouling exposed layer. Nevertheless, a sensitivity study and the sizing probe are achieved thanks to this 3D forward model. However, a simplified 1D forward model was developed in clean and in fouling conditions by considering a homogeneous layer of fouling around the probe.

4.2. Simplified 1D forward model in fouling conditions

The electric equivalent representation of the problem is presented in Fig. 4:

This representation represents the physically simplified model and the different hypotheses made to simplify the model are the following one:

- The insulating layers are considered as only resistive (R_1 and R_2).
- The metal layers are considered as only capacitive (C_s).
- The heater inertia is considered as negligible.
- The cooling water flowing through the inner cylinder sets its temperature.
- The contact resistances are considered as negligible.
- The heat transfer is considered as 1D according to the radial variable r .
- The deposit layer on the probe (R_d and C_d) is assumed to be homogeneous. Its average thermal conductivity is set at $0.07 \text{ W m}^{-1} \text{ K}^{-1}$ and its volumic heat at $3.5 \times 10^5 \text{ J m}^{-3} \text{ K}^{-1}$.

Proceeding in the same way as previously, the temperature response at the level of the heater in real space can be written:

$$T(r_3, t, e_d) = \frac{\varphi(R_1 R_2)}{(R_1 + R_2)} + \underbrace{\left[\frac{\varphi R_d^2 (1 + R_d h 2\pi r_7)}{[1 + h 2\pi r_7 (R_1 + R_2)] (R_1 + R_2)} \right]}_{T_{\text{max}}} \cdot (1 - e^{-t/\tau_d}) \quad \text{with} \quad (18)$$

$$\tau_d = \frac{(R_1 + R_2)(1 + R_d h 2\pi r_7)(C_d + C_s)}{[1 + h 2\pi r_7 (R_1 + R_2)]} = R_{\text{fouling}} C_{\text{fouling}}$$

where τ_d represents the characteristic time constant in fouling conditions. It can be defined by a product of a global resistance by a global capacity.

Such expression can be explained with reduced terms such as:

$$T(r_3, t, e_d) = T_{\text{max}} f\left(\frac{t}{\tau}\right) \quad (19)$$

Both simplified models are an excellent approximation of the 3D model. The heater inertia is more closely considered in the 3D model but there is no influence on the physical phenomena involved.

5. Sensitivity analysis

This probe design was subjected to technological constraints. Indeed, the internal and the external layers are in stainless steel to represent heat exchangers in industrial conditions at best. The sensitivity study enables to impose the various values of the missing parameters such as the thickness of the layers or the nature of the insulating material. This study allows the discussion on the possibility of physical parameters identification.

The reduced sensitivity functions of $T(r_3, x, z, t)$ to parameter η_i will be defined by the following relation [21]:

$$X_{\eta_i}^*(t) = \eta_i \frac{\partial T(r, x, z, t, \eta_i)}{\partial \eta_i} \quad (20)$$

To characterise the fouling evolution around the probe, two parameters in the 3D forward model appear as essential:

- the air sight convective heat transfer coefficient h ;
- the volumic heat variation of the fouling exposed layer due to fouling grow ρC_p which is equivalent to a thickness variation.

Indeed, the fouling involves a modification of these two transfer parameters. To size the probe in order to achieve the best compromise between industrial constraints and sensitivity analysis, it is useful to plot the reduced sensitivity functions of $T(r_3, \forall x, z, t)$ to these two parameters for several values (layer thickness, thermal conductivity, etc.) versus the duration of thermal excitation.

For example, the following two figures (Figs. 5 and 6) represent, respectively, the reduced sensitivity functions to h and to ρC_p according to several values of the thermal conductivity of the

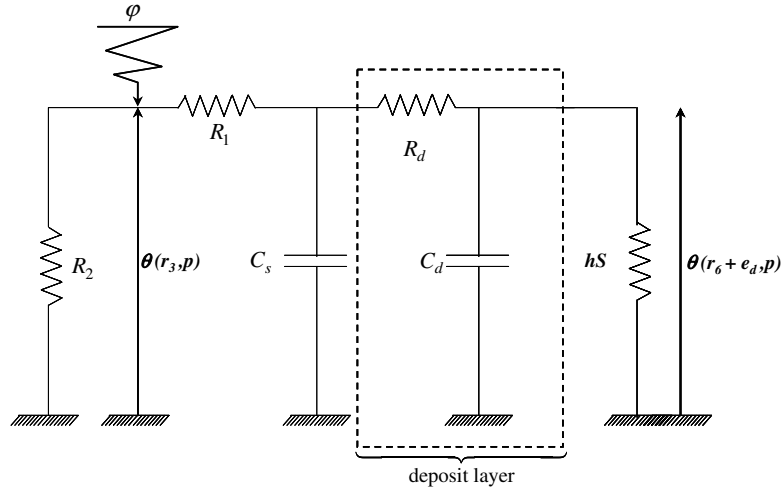


Fig. 4. Electric equivalent representation of the problem in fouling conditions.

closest air sight insulating layer varying from 0.25 to 40 W m⁻¹ K⁻¹ for a duration of thermal excitation of 1000 s.

It is important to note that the higher this thermal conductivity, the more sensitive to ρC_p the temperature measured by the probe (Fig. 5) but it is less sensitive to h (Fig. 6).

So, the available insulating material best answering the various constraints and the sensibilities is the PTFE. In the same way, the various thicknesses of layers were set at 2 mm.

The physical properties of each layer and nominal values are given in Table 1.

Thus, the reduced sensitivity functions of $T(r_3, x, z, t)$ to ρC_p , and to h were calculated from the values of the chosen materials in Table 1. They are plotted in Fig. 7.

This sensitivity study proves that the probe temperature signal is sensitive not only to the convective heat transfer coefficient h but also to the volumic heat of the stainless steel layer subjected to fouling. However, the probe is sensitive to this volumic heat only for a period of time down to 300 s while it is sensitive to the convective heat transfer coefficient on the entire considered temporal domain.

6. Experimental results

To obtain experimental results both in clean conditions and in fouling conditions, the probe is inserted into the testing bench named GAZPAR.

6.1. Experimental sensitivity study in fouling conditions

Before carrying out fouling tests, it is necessary to wait for the thermohydraulic stabilisation of the experimental device GAZPAR. Once this stabilisation reached, foulant particles are produced by ultrasound pulverisation and they are injected into the hot wind tunnel. The tests were performed on a duration going from 13 to 72 h, for an air flow rate of 100 Nm³ h⁻¹ with the air temperature set at 323 K. So, the corresponding Reynolds number calculated from the probe diameter is 7.4×10^3 . The particles dispersion air flow rate is set at 6.7×10^{-8} m³ s⁻¹.

Rather than using the 3D forward model, an experimental sensitivity study from the normalised experimental temperatures $\bar{T}(r_3, t, e_d)$ was performed.

The normalised experimental temperature in fouling conditions $\bar{T}(r_3, t, e_d)$ can be written:

$$\bar{T}(r_3, t, e_d) = \frac{T(r_3, t, e_d)}{T_{\max}} \quad (21)$$

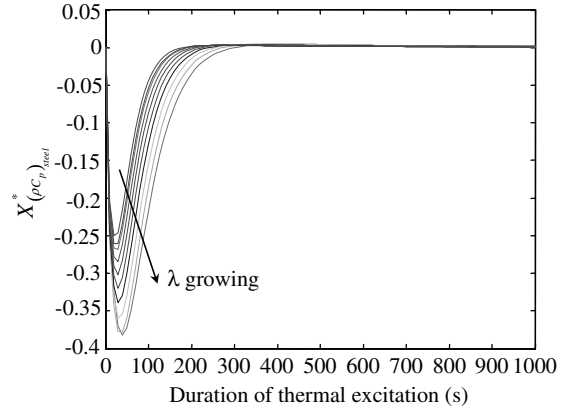


Fig. 5. Reduced sensitivity functions to ρC_p for different values of thermal conductivity.

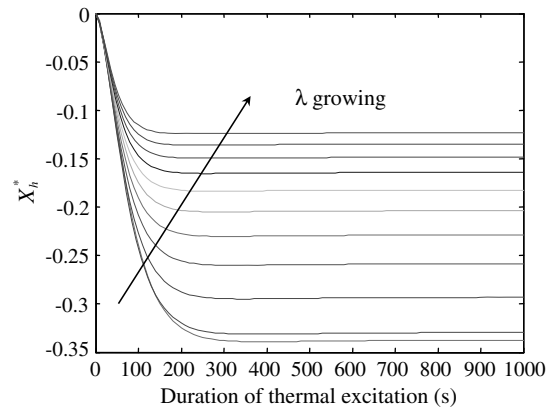


Fig. 6. Reduced sensitivity functions to h for different values of thermal conductivity.

Fig. 8 represents a normalised experimental temperature $\bar{T}(r_3, t)$ in clean conditions and normalised experimental temperatures $\bar{T}(r_3, t, e_d)$ after 72 h of fouling in the same thermohydraulic conditions.

Fig. 8 proves that the deposit formed on the probe only influences the probe characteristic time constant. Indeed, it is logical to assume that the variation of the characteristic time constant is only due to the thickness of the deposit on the probe because its response in temperature is not sensitive to the convective heat

Table 1
Nominal values of the probe

Excitation heat flux	$\varphi = 17,862 \text{ W m}^{-2}$
Stainless steel thermal conductivity	$\lambda_s = 16.3 \text{ W m}^{-1} \text{ K}^{-1}$
Stainless steel specific heat	$\rho C_{ps} = 4 \times 10^6 \text{ J m}^{-3} \text{ K}^{-1}$
Stainless steel layer thickness	$e_s = 2 \times 10^{-3} \text{ m}$
Teflon thermal conductivity	$\lambda_{tef} = 0,25 \text{ W m}^{-1} \text{ K}^{-1}$
Teflon specific heat	$\rho C_{pte} = 2,2 \times 10^6 \text{ J m}^{-3} \text{ K}^{-1}$
Teflon layer thickness	$e_{tef} = 2 \times 10^{-3} \text{ m}$
Heater thickness	$e_h = 0.2 \times 10^{-3} \text{ m}$
Heater width	$b = 0.01 \text{ m}$

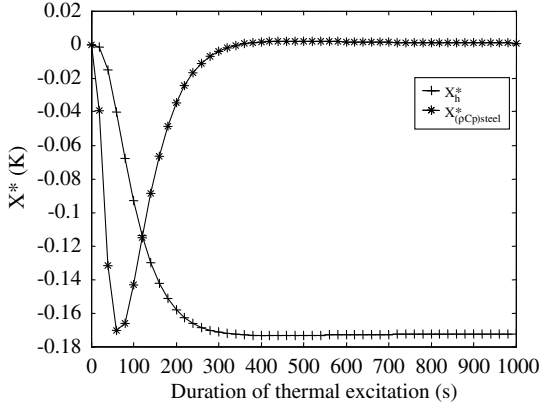


Fig. 7. Reduced sensitivity functions of $T(r_3, x, z, t)$ to ρC_p , and to h .

transfer coefficient in transient state. Then, the fouling appears as a transient information. Consequently, it is possible to write the asymptotic first order development around the probe characteristic time constant. So, it comes:

$$\bar{T}(r_3, t, e_d) = \bar{T}(r_3, t) + \frac{\Delta\tau}{\tau_c} t \frac{\partial \bar{T}(r_3, t)}{\partial t} \quad (22)$$

This first order development is expressed generally under the following way:

$$\bar{T}(r_3, t, e_d) = \bar{T}(r_3, t) + \Delta\tau \frac{\partial \bar{T}(r_3, t)}{\partial t} \quad (23)$$

However, the major drawback of this expression computation lies in the fact that it is necessary to know accurately the nominal values of the problem.

Thus, the experimental sensitivity coefficient in fouling conditions is:

$$X(r_3, t, e_d) = \bar{T}(r_3, t, e_d) - \bar{T}(r_3, t) = \frac{\Delta\tau}{\tau_c} t \frac{\partial \bar{T}(r_3, t)}{\partial t} \quad (24)$$

The different experimental sensitivity coefficients to the fouling for various duration of fouling are plotted in Fig. 9.

These different experimental sensitivity coefficients to the fouling are calculated from all the signal data and not from the nominal values of the problem. One can note the similarity of curves shapes between the experimental and the theoretical sensitivity analysis to fouling (Fig. 10).

6.2. Method of estimation and results in fouling conditions

It is then possible to write the corresponding order -1 moment by integrating the relation (24) as:

$$\begin{aligned} M_{-1} &= \int_{t=0}^{t=t_{\max}} \frac{1}{t} (\bar{T}(r_3, t, e_d) - \bar{T}(r_3, t)) dt \\ &= \int_{t=0}^{t=t_{\max}} \frac{\Delta\tau}{\tau_c} \frac{\partial \bar{T}(r_3, t)}{\partial t} dt \end{aligned} \quad (25)$$

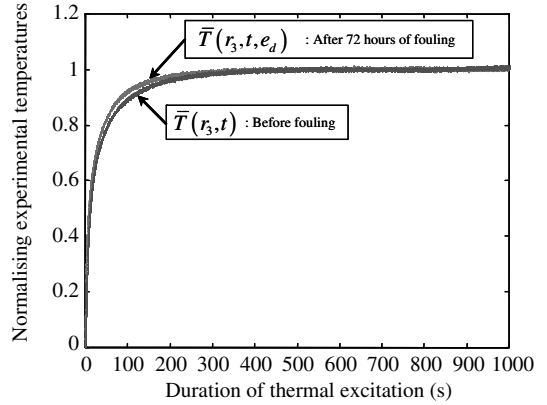


Fig. 8. Normalized experimental temperatures in clean conditions and after 72 h of fouling.

or:

$$M_{-1} = \int_{t=0}^{t=t_{\max}} \left(\frac{X(r_3, t, e_d)}{t} \right) dt \quad (26)$$

Thus:

$$M_{-1} = \int_{t=0}^{t=t_{\max}} \left(\frac{X(r_3, t, e_d)}{t} \right) dt = \frac{\Delta\tau}{\tau_c} \quad (27)$$

So, each -1 order moment can be directly calculated from the experimental sensitivity coefficients for each duration of fouling by a simple integration.

Thanks to the 1D simplified models in clean conditions and in fouling conditions, the probe characteristic time constants τ_c and τ_d can be written as:

$$\tau_c = R \cdot C \quad \text{and} \quad \tau_d = R_{\text{fouling}} \cdot C_{\text{fouling}} \quad (28)$$

where R_{fouling} and C_{fouling} are dependent on the fouling thickness.

Thus, a variation of the deposit thickness on the probe entails a variation of R_{fouling} and of C_{fouling} . It becomes possible to write:

$$\tau_d = \tau_c + \Delta\tau = \left(R + \frac{\Delta e_d}{\lambda_d} \right) \cdot \left(C + (\rho C_p)_d \Delta e_d \right) \quad (29)$$

where λ_d is the thermal conductivity of the deposit and $(\rho C_p)_d$ is its density. So, it comes:

$$\begin{aligned} \frac{\Delta\tau}{\tau_c} &= \left(\frac{(\rho C_p)_d}{\lambda_d R C} \right) (\Delta e_d)^2 + \left(\frac{(\rho C_p)_d}{R} + \frac{1}{\lambda_d C} \right) \Delta e_d \\ &= \beta_1 (\Delta e_d)^2 + \beta_2 \Delta e_d \end{aligned} \quad (30)$$

The -1 order moment obtained from the various experimental sensitivity coefficients is thus proportional to deposit thickness:

$$M_{-1} = \beta_1 (\Delta e_d)^2 + \beta_2 \Delta e_d \quad (31)$$

where $\Delta e_d = (e_d)_{t=t_i} - (e_d)_{t=0}$. The term $(\Delta e_d)^2$ is a two-order term, it could be considered as negligible. First, it is necessary to estimate the coefficients β_1 and β_2 . The problem of estimation can be written as:

$$\underbrace{\begin{bmatrix} (M_{-1})_{t_d=0} \\ \vdots \\ (M_{-1})_{t_d=t_i} \end{bmatrix}}_{[M_{-1}]} = \underbrace{\begin{bmatrix} (\Delta e_d)_{t=0}^2 & (\Delta e_d)_{t=0} \\ \vdots & \vdots \\ (\Delta e_d)_{t=t_i}^2 & (\Delta e_d)_{t=t_i} \end{bmatrix}}_{[X]} \underbrace{\begin{bmatrix} \beta_1 \\ \beta_2 \end{bmatrix}}_{[\beta]} \quad (32)$$

If the noise is correlated or not a constant deviation during time, the Gauss-Markov method can be used as:

$$[\beta] = [X]^t \text{cov}(e_{M_{-1}})^{-1} [X]^{-1} [X]^t \text{cov}(e_{M_{-1}})^{-1} [M_{-1}] \quad (33)$$

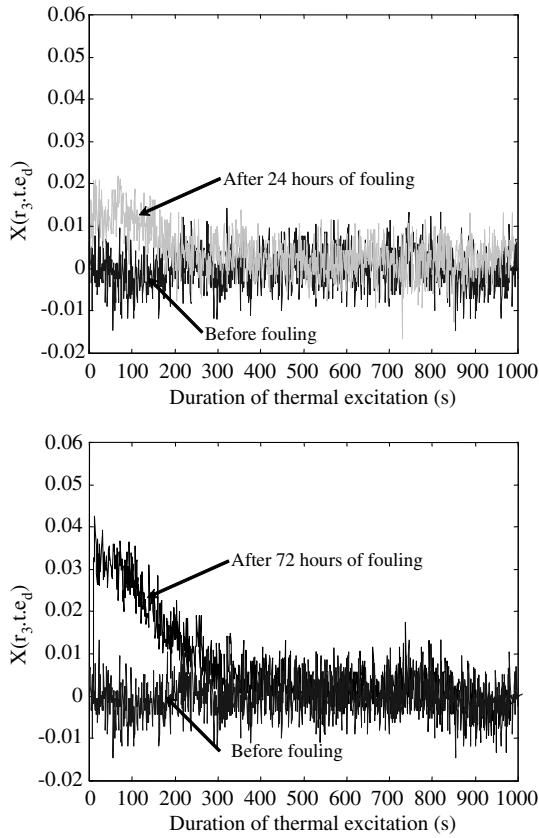


Fig. 9. Experimental sensitivity coefficients to fouling for various duration of fouling.

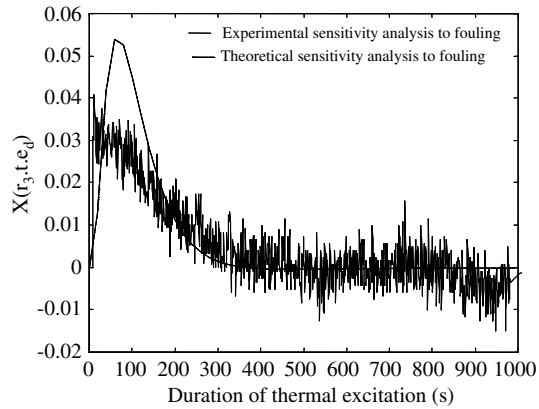


Fig. 10. Comparison between experimental and theoretical sensitivity coefficients to fouling.

where $\text{cov}(e_{M-1})$ represents the covariance matrix of the noise measurement.

The interest of this estimation lies in the fact that it is not greatly dependent on the considered forward model and on the nominal values of the problem. Indeed, the experimental sensitivity coefficients are calculated from the signal and not from the nominal values of the considered forward model.

Once the tests in fouling conditions were completed, the deposit pattern around the probe for each considered duration of fouling is measured by a laser profiler. These are plotted in Fig. 11. For the considered fouling conditions, various deposit regimes such as the inertial impaction and the turbulent diffusion

occur. This comment explains why the measured deposit pattern is not homogeneous around the probe. Every average deposit thickness is calculated by integrating these values by the trapeze method.

Because of the limited volume of the sulphate sodium solution tank supplied the particles generator, the fouling tests were performed within a maximal duration of 72 h. So, it is difficult to estimate accurately the parameters β_1 and β_2 . However, as the -1 order moments are independent on the considered forward model and on the associated nominal values, it becomes possible to calculate β_1 and β_2 from the sensitivity coefficients obtained from the 1D simplified models.

These two simplified forward model responses have been numerically noise-added before calculating the theoretical -1 order moment which has allowed obtaining the corresponding standard deviation.

So, Fig. 12 represents the experimental and theoretical -1 order moments and their associated standard deviation. The -1 order moments obtained from the 3D forward model are also plotted in this figure.

This figure shows that the -1 order moments are no dependent on the considered forward model and on the nominal values of the problem. Besides, it shows that the noise is not correlated and that the -1 order moments are obtained accurately. So, from the -1 order moment values and from Eq. (33), it is possible to estimate the parameters β_1 and β_2 . From these parameter values and from the knowledge of the experimental -1 order moment for a duration of fouling, the deposit thickness around the probe can be calculated such as:

$$\Delta e_d = e_d = \frac{-\beta_2 + \sqrt{\Delta}}{2\beta_1} \quad \text{with} \quad \Delta = (\beta_2)^2 + 4\beta_1 M_{-1} \quad (34)$$

Afterward, from the knowledge of the convective heat transfer coefficient in clean conditions, from the knowledge of the average deposit thicknesses around the probe, the conductance in fouling conditions can be calculated by:

$$\left(\frac{1}{h}\right)_d = \left(\frac{1}{h}\right)_c + \frac{e_d}{\lambda_d} \quad (35)$$

where $\lambda_d = 0.07 \text{ W m}^{-1} \text{ K}^{-1}$.

7. Conclusions

A transient thermal fouling probe was designed to replace one part or the totality of heat exchanger tubes. This probe becomes representative of the thermohydraulic and fouling conditions as heat exchangers whereas classical methods tend to characterise the phenomenon involved too late for relevant use.

The principle of the method is linked to the processing of transient temperature elevations carried out by a heater inside the tube wall.

An experimental sensitivity study was implemented in order to estimate not only the average heat transfer coefficient but also the average fouling thickness around the tube. The sensitivity coefficients are obtained from the temporal variation of the experimental temperatures and not from the nominal values of the forward model as they usually are.

The validation of the device was performed in a calibrated environment and the fouling thickness was verified with optical measurements.

This probe has shown its capacity to allow the determination of the convective heat transfer coefficient in clean conditions and the determination of the deposit thickness around the heat exchanger in fouling conditions from a new method of estimation.

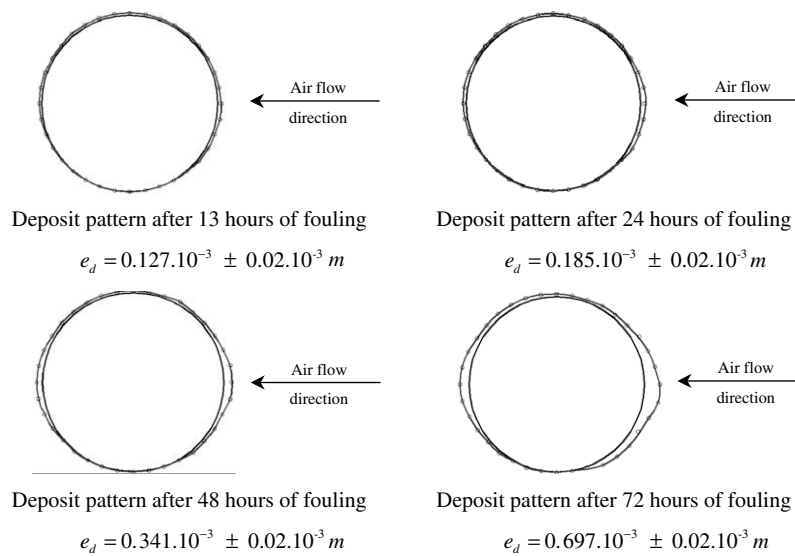


Fig. 11. Deposit pattern for different duration of fouling.

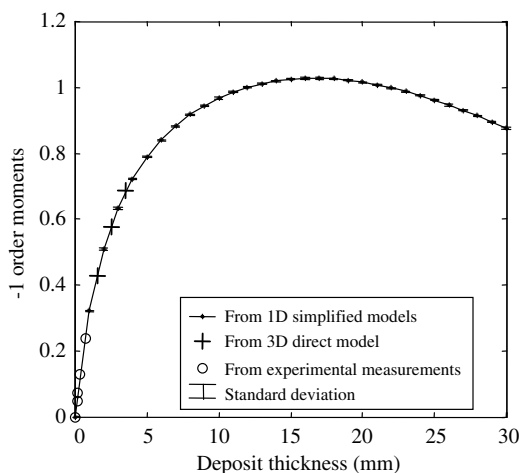


Fig. 12. Various -1 order moments versus deposit thickness.

The results were successfully confronted with the data available from the literature and with the experimental measurements obtained optically.

The advantages of such a device are to be cheap, localised and technologically simple associated with adapted data processing. The transient state estimation method developed is robust. It is not greatly dependent on noise measurement and on the nominal values of the problem.

The perspectives of this work are to extend the method to other exchanger technologies (liquid–liquid, plate heat exchangers, etc.) and other fouling conditions (corrosion, scaling, etc.).

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